



HAL
open science

Pilot-scale assessment of the viability of UVA radiation for H₂O₂ or S₂O₈²⁻ activation in advanced oxidation processes

Anaëlle Gabet, Christine de Brauer, Gilles Mailhot, Marcello Brigante, H  l  ne M  tivier

► To cite this version:

Ana  lle Gabet, Christine de Brauer, Gilles Mailhot, Marcello Brigante, H  l  ne M  tivier. Pilot-scale assessment of the viability of UVA radiation for H₂O₂ or S₂O₈²⁻ activation in advanced oxidation processes. *Journal of Water Process Engineering*, 2023, 56, pp.104328. 10.1016/j.jwpe.2023.104328 . hal-04283686

HAL Id: hal-04283686

<https://uca.hal.science/hal-04283686>

Submitted on 19 Nov 2023

HAL is a multi-disciplinary open access archive for the deposit and dissemination of scientific research documents, whether they are published or not. The documents may come from teaching and research institutions in France or abroad, or from public or private research centers.

L'archive ouverte pluridisciplinaire **HAL**, est destin  e au d  p  t et    la diffusion de documents scientifiques de niveau recherche, publi  s ou non,   manant des   tablissements d'enseignement et de recherche fran  ais ou   trangers, des laboratoires publics ou priv  s.

1 **Pilot-scale assessment of the viability of UVA radiation for H₂O₂ or S₂O₈²⁻**
2 **activation in advanced oxidation processes**

3 Anaëlle Gabet^{1,2}, Christine de Brauer¹, Gilles Mailhot², Marcello Brigante², H el ene
4 M etivier^{1,*1}

5
6 ¹ Univ Lyon, INSA Lyon, DEEP, EA7429, 69621 Villeurbanne, France

7 ² Universit e Clermont Auvergne, CNRS, Clermont Auvergne INP, Institut de Chimie de
8 Clermont-Ferrand, F-63000 Clermont-Ferrand, France

9
10 **Abstract**

11 UVA and UVC radiation were compared for the activation of H₂O₂ or S₂O₈²⁻ to remove
12 micropollutants remaining in treated wastewater with a view to optimising the cost and/or the
13 efficiency of the commonly studied UVC/H₂O₂ process. Experiments were carried out in a
14 dynamic laboratory pilot (20 L). In a simple matrix, UVA radiation were able to produce
15 oxydative radicals from H₂O₂ or S₂O₈²⁻, although faster degradation of the estrogens was
16 observed under UVC radiation (up to 55-fold). With both UV radiation, S₂O₈²⁻ was
17 photolyzed faster than H₂O₂, resulting in faster estrogen degradation (up to 12-fold). Coupling
18 UVA to H₂O₂ was considered not to be viable because less than 4% of the compounds were
19 degraded at 1000 mJ cm⁻². In a treated wastewater, estrogen degradations were inhibited due
20 to organic matter and stronger inhibitions were observed with S₂O₈²⁻ processes (up to 80%
21 inhibition compared to simple matrix). The UVC/S₂O₈²⁻-process still achieved the fastest
22 degradation rate, but is roughly comparable to the UVC/H₂O₂-process. Very low degradation
23 rates obtained with UVA/S₂O₈²⁻ limit the interest in the process. Experiments were also
24 carried out on a mixture of pharmaceuticals leading to similar conclusions.

* corresponding author. [Tel:+33-472-436-288](tel:+33-472-436-288). E-mail: helene.metivier@insa-lyon.fr

25

26 **Keywords:** AOPs, micropollutants, photolysis, pilot scale, UVA radiation, wastewater.

27

28 **1. Introduction**

29 Water scarcity is about to be one of the major challenges of the next decades. The European
30 Union Water Framework Directive adopted in 2000 aims at protecting the quality and the
31 quantity of water bodies in the European Union. Although significant improvements were
32 observed within the last decades regarding the quality of water bodies, the presence of
33 anthropogenic micropollutants in surface and ground waters is increasingly reported.
34 Wastewater treatment plants (WWTPs), whether they are conventional or wetlands, are one of
35 the major gateways of micropollutants to the environment because a large panel of
36 compounds is refractory to the treatments that are commonly used. As a consequence,
37 effluents are released to the environment with micropollutants at concentrations up to several
38 tens of $\mu\text{g L}^{-1}$ [1, 2, 3]. Improving the removal of micropollutants in WWTPs by the use of
39 appropriate treatments would allow the discharge of water of better quality. Moreover, it
40 could promote effluent reuse for crop fields irrigation or industrial use for example and
41 decrease the pressure on aquatic environments.

42 In France, more than 90% of the WWTPs are small and medium-sized (< 10,000 population
43 equivalent) and around 40% are equipped by nature-based processes such as constructed
44 wetlands (CWs) [4]. These plants have different human and technical resources and therefore
45 different needs compared to large-scale urban WWTPs. They require cheap, reliable and low-
46 maintenance processes. Among the existing treatments for micropollutants, photoactivated
47 advanced oxidation processes (AOPs) seem to meet these criteria. They consist in the
48 generation of highly oxidising species such as HO^\bullet ($E_{\text{HO}^\bullet/\text{HO}^-}^0 = 2.80 \text{ V/SHE}$ at 25 °C) by the
49 photolysis of an oxidant precursor (typically H_2O_2). The abilities of the UVC/ H_2O_2 process

50 have been widely reported. Cédat et al. [5] observed the complete degradation of a mixture of
51 three estrogens (5 μM each spiked in a WWTP effluent) and of their estrogenic activity and
52 estimated the cost of the technology to be under 0.20 € m^{-3} . However, UVC radiation is
53 generally produced by mercury lamps which are quite energy consuming. In the UVC/H₂O₂
54 process, Cédat et al. [5] estimated that electricity would represent from 14 to 38% of the total
55 treatment cost. Moreover, H₂O₂ supply is another significant expenditure item since it was
56 estimated to represent from 47 to 62% of the total cost.

57 With a view to optimising the efficiency/cost ratio of the AOP, alternatives to the UVC/H₂O₂
58 treatment were presented in the literature. For example, the abilities of S₂O₈²⁻ as an oxidant
59 precursor to generate two sulfate radicals (SO₄^{•-}) ($E_{SO_4^{\bullet-}/SO_4^{2-}}^0 = 2.5 - 3.1 \text{ V/SHE}$ at 25 °C,
60 depending on the solution pH) by photolysis have been widely shown [6, 7, 8].

61 Then, another alternative is the use of solar light as a UV source. Incident solar radiation on
62 earth is a free and renewable energy, composed of 95% of UVA and 5% of UVB and it was
63 previously reported in the literature that UVA radiation is able to photolyse H₂O₂ and S₂O₈²⁻
64 [9, 10]. Fernandes et al. [11] also recently demonstrated that natural solar radiation is efficient
65 in activating these oxidant precursors. Kowalska et al. [12] and Moreira et al. [10] observed
66 complete degradation of carbamazepine and diclofenac in spiked effluents under solar
67 radiation coupled to H₂O₂. Finally, Rizzo et al. [13] and Velo-Gala et al. [14] both compared
68 the efficiency of a solar simulator to UVC radiation for the activation of H₂O₂ in order to
69 degrade antibiotics in small volumes (0.5 and 6 L respectively). In both studies, the lower
70 efficiency of solar light compared to UVC radiation was concluded. However, the reported
71 degradation rates were time-dependent and no comparison of the energy required (UV
72 fluence) in each process was made.

73 Since UVA radiation constitute the majority of solar UV, it seems essential to evaluate their
74 abilities for the activation of oxidant precursors in AOPs. To the best of our knowledge, no

75 previous study has compared UVA to UVC radiation for the photo-activation of H₂O₂ and
76 S₂O₈²⁻.

77 In the present work, an intermediate-scale laboratory pilot (maximum capacity of 50 L) was
78 used to compare UVA to UVC radiation for the activation of H₂O₂ or S₂O₈²⁻. H₂O₂ was
79 chosen for its ease of implementation and the large number of studies identified in the
80 literature. S₂O₈²⁻ was studied for its high efficiency with the aim of assessing whether its use
81 could balance the expected loss of efficiency when replacing UVC by UVA radiation. For
82 technical reasons, mercury lamps were used for the production of both types of radiation,
83 allowing UV fluence calculation and comparison. Three estrogens, namely estrone (E1),
84 17β-estradiol (E2) and 17α-ethinylestradiol (EE2), were first chosen as model pollutants for
85 process efficiency assessment. According to Ilyas and van Hullebusch [15], they are removed
86 from 30 to 80% in constructed wetlands, due to biodegradation, plant uptake and adsorption,
87 leading to concentrations from ng L⁻¹ to several μg L⁻¹ in the released effluent. Similar
88 degradation rates are also achieved in conventional WWTPs [16, 17]. Nevertheless, their
89 occurrence in surface waters and river sediments as well as their ecotoxicity at environmental
90 concentrations have been widely reported [18]. Finally, a mixture of ibuprofen, (IBU),
91 naproxen (NAP) and diclofenac (DCF), three commonly detected non-steroidal anti-
92 inflammatory drugs, allowed to confirm the results on another type of micropollutants.

93 **2. Materials and methods**

94 *2.1. Chemicals and reagents*

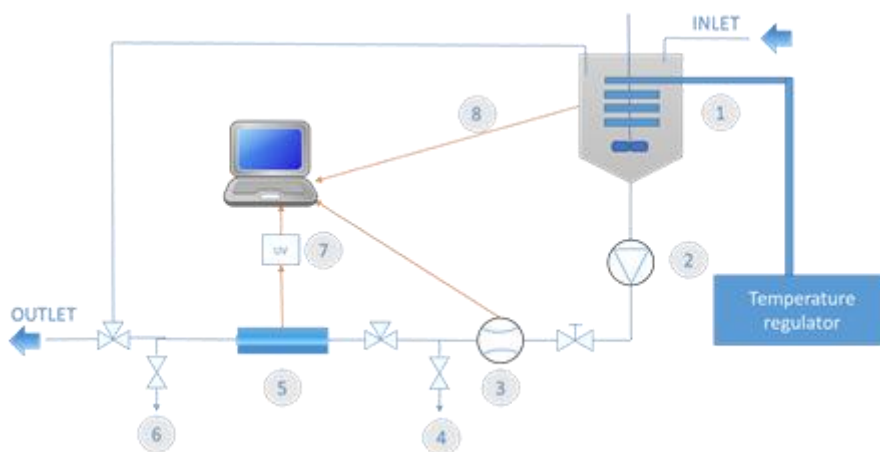
95 Estrone (E1), 17β-estradiol (E2), 17α-ethinylestradiol (EE2), ibuprofen (IBU) sodium salt,
96 diclofenac (DCF) sodium salt and naproxen (NAP) were purchased from Sigma-Aldrich, as
97 well as H₂O₂ (30% in water) and Na₂S₂O₈. Persulfate stock solutions were prepared in
98 drinking water (1 M). E1, E2, EE2 and NAP stock solutions were prepared at 5 mM in
99 acetonitrile. IBU and DCF stock solutions were made at 10 mM in drinking water.

100 Acetonitrile (ACN) was supplied by VWR Chemicals (HPLC grade). Ultrapure water was
101 obtained from a milli-Q system. Formic acid was purchased from Chimie-plus Laboratoires.

102 2.2. Irradiation experiments

103 2.2.1. Description of the laboratory pilot

104 The experimental set-up has previously been described in the literature (Cédât et al., 2016)
105 and is reproduced Figure 1. It is composed of a 50-L glass tank linked to a 1.12-L UV reactor
106 (COMAP) by a centrifugal pump. In the reactor, the UV lamp is protected by a quartz tube
107 and the effluent flows through a 1-cm layer around the tube. Effluent recirculation allows to
108 increase the contact time between the targets and the lamp and thus the UV fluence. Low
109 pressure mercury lamps (Philips) were used for the generation of UVC and UVA radiation.
110 The UVC lamp was monochromatic while the UVA lamp was polychromatic and emits from
111 345 to 410 nm with a maximum at 365 nm (Figure SM1). Their technical features are
112 presented in Table 1.



113
114 Figure 1. Schematic diagram of the pilot used, reproduced from Cédât *et al.*, 2016. 1) Glass tank; 2) pump; 3)
115 flow meter; 4) and 6) sampling points; 5) UV reactor; 7) UV intensity control; 8) temperature control.

116

117 Table 1. Technical characteristics of UVA and UVC lamps.

UV type	Lamp power (W)	Power efficiency	Wavelength (nm)	Length (cm)	Hg (mg)
UVC	54	32%	254	60.0	8.0
UVA	36	24%	345 – 410	89.5	2.0

118 The UVCalc®2A software (Bolton Photosciences Inc., Canada) was used for UV fluence
 119 calculations. On the advice of the software designer and given its narrow emission spectra, the
 120 UVA lamp was considered monochromatic. After calculation, a correction factor of 0.88 for
 121 UVC radiation [5] and 0.82 for UVA radiation (software designer recommendations) was
 122 applied.

123 2.2.2. Matrix composition

124 Main physico-chemical parameters of the matrices used to investigate the degradation of
 125 micropollutants are presented in Table 2. Drinking water collected directly to tap
 126 (Villeurbanne, France) was first used as a simple matrix. Then, WWTP effluents were
 127 collected in 30-L plastic containers at the outlet of a conventional WWTP equipped by an
 128 activated sludge treatment (Feyssine, Villeurbanne, France) with a capacity of 300,000
 129 population equivalent. Samples were collected in the morning and used within 30 hours.

130 Table 2. Main physico-chemical parameters of drinking water and WWTP effluents.

	Drinking water	WWTP effluent 1	WWTP effluent 2
pH	7.7	7.8	7.9
UV _{254nm} transmittance	98%	62%	61%
UV _{365nm} transmittance	> 99%	90%	87%
Conductivity ($\mu\text{S cm}^{-1}$)	395	913	912
Suspended solids (mg L^{-1})	-	4	4
Chemical Oxygen Demand (COD) (mg L^{-1})	< 5	29	26
Total Organic Carbon (TOC) ($\text{mg}_C \text{L}^{-1}$)	-	7.5	5.8
Cl ⁻ (mg L^{-1})	10	107	98
NO ₃ ⁻ (mg L^{-1})	5.1	21.2	24.6
HCO ₃ ⁻ (mg L^{-1})	220	208	252

131 2.2.3. Experimental procedures

132 The laboratory pilot was used to determine the photolysis constants of the oxidant precursors,
 133 the photolysis first order rate constants of the estrogens and the overall pseudo-first order
 134 degradation rate constant of the estrogens or of the pharmaceuticals obtained through the
 135 experiments. Experimental procedures were quite similar and operating conditions are

136 summarized in Table 3. The experimental set-up was filled in to 20 ± 0.5 L with the matrix.
137 Then, recirculation flow was set at 20 ± 0.5 L min^{-1} , the UV lamp was pre-heated during
138 10 minutes and the temperature was adjusted and stabilised at 22 ± 2 °C. After pre-heating,
139 the lamp was turned off and the solution was spiked with 3 estrogens or 3 pharmaceuticals at
140 $5 \mu\text{M}$ each (except for the experiments regarding oxidant precursor photolysis). Although this
141 concentration is higher than those in WWTP effluents, it does not require pre-concentration
142 prior to ultra high-performance liquid chromatography (UHPLC) analysis and therefore
143 allows the sampling of small volumes, suitable for kinetic experiments. Then, an appropriate
144 volume of oxidant precursor was added: 10.3 mL of H_2O_2 (30%) or 100 mL of a 1 M $\text{S}_2\text{O}_8^{2-}$
145 stock solution were added to reach a concentration of 5 mM ; 2.06 mL of H_2O_2 (30%) and 20
146 mL of $\text{S}_2\text{O}_8^{2-}$ 1 M were added to reach a concentration of 1 mM. No oxidant precursor was
147 added for estrogen photolysis experiments. For oxidant precursor photolysis only, 100 mL of
148 methanol (0.5% v/v) were also added: methanol quenches the newly formed hydroxyl or
149 sulfate radicals to prevent them from reacting in turn with H_2O_2 or $\text{S}_2\text{O}_8^{2-}$.

150 After addition of the reagents, the solution was homogenised for 2 minutes and the lamp was
151 turned on to start the experiment. 5 mL were withdrawn before the start and at the end of each
152 experiment to measure the transmittance of the solution by UV-visible spectrophotometry.
153 During estrogen photolysis and AOP experiments, 1 mL of sample was withdrawn at fixed
154 time intervals for micropollutant quantification by UHPLC. During H_2O_2 or $\text{S}_2\text{O}_8^{2-}$ photolysis
155 experiments, the volume of samples was extended to 5 mL to determine their concentrations
156 using a UV-visible spectrophotometer.

157 In any case, variations between the initial and the final volume were under 0.25% during
158 experiments.

159

Table 3. Operating conditions in the pilot.

	Photolysis experiments		UV-based AOP experiments	
	Oxidant precursors	Estrogens	Estrogens	Pharmaceuticals
Total volume	20 ± 0.5 L			
Recirculation flow rate	20 ± 0.5 L min ⁻¹			
Solution	Drinking water	Drinking water	Drinking water or WWTP1	WWTP2
Micropollutants	None	E1 + E2 + EE2 5 µM each	E1 + E2 + EE2 5 µM each	IBU + NAP + DCF 5 µM each
Oxidant precursor	H ₂ O ₂ or S ₂ O ₈ ²⁻ 5 mM	None	H ₂ O ₂ or S ₂ O ₈ ²⁻ 1 mM	H ₂ O ₂ or S ₂ O ₈ ²⁻ 1 mM
Methanol	0.5% V/V	None	None	None

161 *2.3. Sample analysis*162 *2.3.1. UV-visible spectrophotometry*

163 A Shimadzu 2450 UV-visible spectrophotometer was used to:

164 - measure transmittances at 254 nm and 365 nm (required for UV fluence calculation),

165 - acquire the UV-visible spectra of the micropollutants and of the oxidant precursors,

166 - quantify H₂O₂ and S₂O₈²⁻ during photolysis constant determination, using167 measurements carried out at 240 nm ($\epsilon_{240\text{nm}} = 38.1 \text{ L mol}^{-1} \text{ cm}^{-1}$) and 230 nm ($\epsilon_{230\text{nm}} = 38.6 \text{ L}$ 168 $\text{mol}^{-1} \text{ cm}^{-1}$) for H₂O₂ and S₂O₈²⁻ respectively.169 *2.3.2. Micropollutant quantification*

170 Samples were filtered before analysis through 0.45 µm PVDF filters (Millex HV). Analysis

171 were performed with an UHPLC ultimate 3000+ (Thermo Fischer) system equipped with a

172 X-Bridge BEH column (75 × 4.6 mm × 2.5 µm) and coupled to a diode array detector. The

173 mobile phase was a mixture of acetonitrile (ACN) and milli-Q water both acidified with 0.1%

174 formic acid running in isocratic mode at 1.5 mL min⁻¹. One method was used to analyse the

175 estrogens and another to analyse the mixture of pharmaceuticals. They are both described in

176 Table 4. Limits of detection (LOD) were determined by calculation and limits of

177 quantification were calculated as $3.3 \times \text{LOD}$. All the samples were analysed in duplicate.
178 Examples of typical chromatograms are available in Figure SM2.

179 Table 4. UHPLC method parameters for micropollutant quantification.

UHPLC method	Estrogen method			Pharmaceutical method		
	E1	E2	EE2	IBU	NAP	DCF
Pollutant						
Mobile phase ACN/H ₂ O	50/50			60/40		
Injection volume (μL)	40			20		
Column temperature (°C)	40			40		
Detection wavelength (nm)	280			226	226	281
Retention times (min)	1.91	1.44	1.71	2.02	1.17	1.76
Limit of detection (μM)	0.28	0.25	0.26	0.12	0.10	0.09

180 2.4. Data processing

181 2.4.1. UV fluence

182 UV fluence (F , mJ cm^{-2}) corresponds to the total radiant energy incident from all directions
183 onto an infinitesimally small sphere of cross-sectional area dA , divided by dA according to
184 Bolton and Stefan [19]. In the studied system, the infinitesimally small sphere of cross-
185 sectional area can be considered to be the targeted micropollutants or the oxidant precursors.
186 UV fluence is based on the characteristics of the lamp but also on the structure of the system
187 and on the transmittance of the effluent. Thus, it allows to compare different lamps, processes
188 or effluents. In the present study, UV fluence was used as a reference unit for degradation
189 rates.

190 2.4.2. Degradation rate constants

191 Photolysis of the estrogens and of the oxidant precursors followed first order rates that were
192 fitted by the following equation: $\ln \frac{C}{C_0} = -k'_p F$, where C_0 and C are respectively the initial
193 concentration and the concentration at UV fluence F of the compound of interest (μM) and
194 k'_p the photolysis first order rate constant ($\text{cm}^2 \text{mJ}^{-1}$) which depends on the UV fluence
195 received by the effluent.

196 In AOPs, micropollutant degradation followed pseudo-first order rates. Targets can be
197 degraded by both photolysis and oxidation by the free radicals. In the present study, the

198 radicals are HO[·] or SO₄^{·-}, generated by the homolytic cleavage of H₂O₂ or S₂O₈²⁻ respectively
199 (each of them generates two identical radicals). The two modes of degradation can be
200 distinguished in the following pseudo-first order rate equation, as proposed by Sharpless et
201 Linden [20] :

202 $\ln \frac{C}{C_0} = -(k'_p + k'_{ox})F = -k'F$, where k'_{ox} is the pseudo-first order rate constant of
203 radical-based oxidation and k' is the overall pseudo-first order rate constant. k'_{ox} depends on
204 both the steady-state concentration of the radical and on the second order reaction rate
205 between the oxidative radical and the compound of interest [21]. In the present study, k'
206 values were determined from UV-based AOP experiments and k'_{ox} values were calculated as
207 the difference between k' and k'_p .

208 The error bars associated to degradation constants equal to 3σ , derived from the scattering of
209 the experimental data around the fit curves (intra-series variability).

210 2.4.3. Electrical energy per order

211 The Electrical Energy per Order (E_{EO}) is the electrical energy (kWh) necessary to reduce the
212 concentration of a contaminant by one order of magnitude in one m³ of effluent [22] (Bolton
213 *et al.*, 2001). It is often calculated according to the following equation [23, 24]: $E_{EO} =$

214 $\frac{P \cdot t \cdot 1000}{V \cdot \log\left(\frac{C_i}{C_f}\right)}$, where P is the lamp power (kW), t is the time of irradiation (h), V is the volume of

215 treated effluent (L), C_i and C_f are the initial and final concentrations of the target molecule
216 (expressed in $\mu\text{mol L}^{-1}$ in this paper). This quantity is a useful indicator for comparing
217 photoactivated processes. It is generally considered that a photoactivated process may be
218 economically feasible if its E_{EO} value is less than 10 kWh m⁻³ order⁻¹ [25].

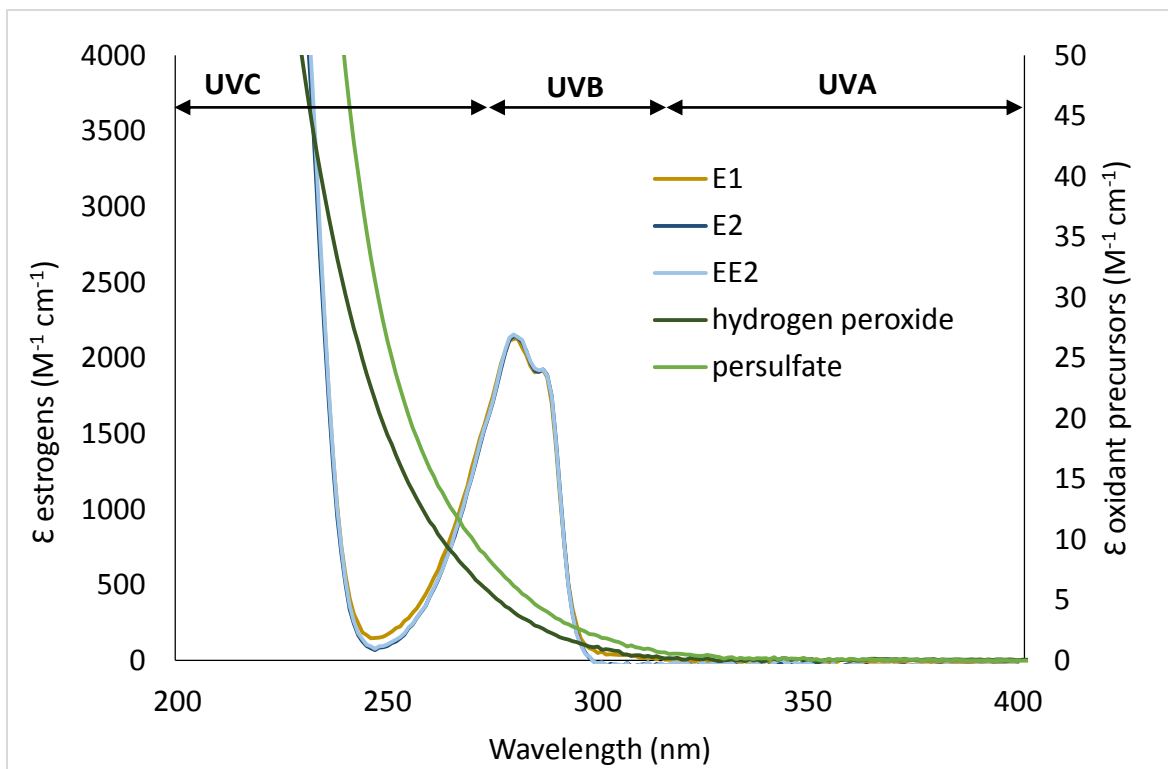
219 Experimental data used to calculate E_{EO} can be seen in Table SM1, only E_{EO} values are
220 presented in the Results and discussion section.

221 3. Results and discussion

222 *3.1. Estrogen and oxidant precursor photolysis*

223 The molar absorption coefficient (ϵ_λ) and the quantum yield (Φ_λ) are the two parameters that
224 account for the photolysis efficiency of a compound. The molar absorption coefficient
225 governs the absorption of a photon by the molecule at the wavelength of interest and the
226 photolysis quantum yield (number of photolysed molecules divided by the number of photons
227 absorbed) depends on the photochemical change that follows photon absorption [26]. Thus,
228 the photolysis quantum yield influences the quantum yield for the generation of photolysis by-
229 products. In the present paper, the modelling of degradation kinetics is not based on these two
230 parameters, but they are used to comment qualitatively on the degradation constants
231 calculated from experimental data.

232 Molar absorption coefficients of H_2O_2 and $\text{S}_2\text{O}_8^{2-}$ and of the targeted estrogens (E1, E2 and
233 EE2) within the UV range are depicted in Figure 2. Molar absorption coefficients at the
234 wavelengths of interest and quantum yields for the production of HO^\bullet and $\text{SO}_4^{\bullet-}$ (from H_2O_2
235 and $\text{S}_2\text{O}_8^{2-}$ photolysis, respectively) found in the literature are reported in Table 5. No
236 quantum yield values for the production of both radicals at 365 nm (maximum emission
237 wavelength of the UVA lamp) were found in the literature, so the values reported in Table 5
238 correspond to the wavelength found closest to 365 nm, i.e. 351 nm. As shown by Hermann
239 (2007), quantum yield decreases with increasing the wavelength of the photolysis light. This
240 decrease is barely noticeable in the case of HO^\bullet formation with quantum yield values from 1.0
241 to 0.96 when wavelength varies from 254 to 351 nm while it is much more significant in the
242 case of $\text{SO}_4^{\bullet-}$ formation with quantum yield values from 1.4 to 0.5 in the same range of
243 wavelength. It can therefore be assumed that $\Phi_{365\text{nm}}(\text{HO}^\bullet) \approx \Phi_{351\text{nm}}(\text{HO}^\bullet)$ while $\Phi_{365\text{nm}}(\text{SO}_4^{\bullet-})$
244 $< \Phi_{351\text{nm}}(\text{SO}_4^{\bullet-})$ so that the ratio $\Phi_{365\text{nm}}(\text{HO}^\bullet) / \Phi_{365\text{nm}}(\text{SO}_4^{\bullet-})$ can be considered greater than 1.9
245 for the comparison of quantum yields for the two radicals under UVA. Under UVC, the ratio
246 $\Phi_{254\text{nm}}(\text{HO}^\bullet) / \Phi_{254\text{nm}}(\text{SO}_4^{\bullet-})$ equals 0.8.



247

248 Figure 2. Molar absorption coefficients (ϵ) of E1, E2 and EE2 and of H_2O_2 and $\text{S}_2\text{O}_8^{2-}$ in the UV range at
 249 circumneutral pH.

250 Table 5. Molar absorption coefficients (ϵ) of estrogens and oxidant precursors and quantum yields for radical
 251 production (Φ) from the photolysis of oxidant precursors under UVC and UVA.

	ϵ ($\text{M}^{-1} \text{cm}^{-1}$)						Φ (mol ein^{-1})	
	H_2O_2	$\text{S}_2\text{O}_8^{2-}$	E1	E2	EE2		HO^\bullet	$\text{SO}_4^{\bullet-}$
UVA (365 nm)	< 0.3	< 0.5	< 10	< 10	< 10	UVA (351 nm)	$0.96 \pm 0.04^{[27]}$	$0.5 \pm 0.1^{[27]}$
UVC (254 nm)	15.4	21.3	261	175	175	UVC (254 nm)	$1.15 \pm 0.05^{[28]}$	$1.4 \pm 0.1^{[29]}$

252

253 3.1.2. Photolysis rate constants of the oxidant precursors

254 As seen in Figure 2, molar absorption coefficients follow the same trend in the UV range for
 255 both H_2O_2 and $\text{S}_2\text{O}_8^{2-}$: they are not significant between 400 and 350 nm and increase
 256 exponentially from 350 to 200 nm. According to Table 5, both oxidant precursors allow
 257 higher quantum yields for the production of free radicals under UVC than under UVA
 258 radiation. Therefore, although it was reported in the literature that UVA radiation is efficient

259 for their activation [9, 30], faster photolysis is expected under UVC radiation for both
260 molecules.

261 At 254 nm, the molar absorption coefficient of $S_2O_8^{2-}$ is 1.4 times higher than that of H_2O_2
262 and the quantum yield for the production of $SO_4^{\cdot-}$ is 1.2 times higher than that of HO^{\cdot} (Table
263 5). Therefore, faster production of $SO_4^{\cdot-}$ is expected. At 365 nm, a higher quantum yield for
264 the production of HO^{\cdot} is expected compared to $SO_4^{\cdot-}$, as suggested by values reported in the
265 literature at 351 nm. However, molar absorption coefficients were too low to be determined,
266 not allowing for the assessment of photolysis outcomes.

267 Photolysis first order rate constants of H_2O_2 and $S_2O_8^{2-}$ in the experimental facility are
268 reported in Table 6. As expected, they are higher under UVC than under UVA radiation (3.5
269 and 8.8 times for H_2O_2 and $S_2O_8^{2-}$ respectively), causing faster generation of the subsequent
270 free radicals under UVC radiation. The photolysis of $S_2O_8^{2-}$ is about 1.2 and 3.4 times faster
271 than that of H_2O_2 , under UVA and UVC radiation respectively. Therefore, the generation of
272 $SO_4^{\cdot-}$ is expected to be faster than that of HO^{\cdot} regardless of the wavelength.

273 Table 6. Photolysis first order rate constants (k'_p) of H_2O_2 and $S_2O_8^{2-}$ in the system.

	k'_p ($cm^2\ mJ^{-1}$)	
	H_2O_2	$S_2O_8^{2-}$
UVA	$4.36 \pm 0.30 \times 10^{-5}$	$5.25 \pm 0.51 \times 10^{-5}$
UVC	$1.54 \pm 0.02 \times 10^{-4}$	$4.61 \pm 0.26 \times 10^{-4}$

274 3.1.3. Photolysis of the estrogens

275 According to Figure 2, E1, E2 and EE2 molar absorption coefficients are very similar at all
276 wavelengths. They have a similar absorption band from 300 to 250 nm and molar absorption
277 coefficients increase exponentially in a similar way from 250 to 200 nm. However, at 254 nm,
278 ϵ is 1.5 times higher for E1 than for E2 and EE2. Moreover, according to Huang et al. [31],
279 E1 has a 3 to 4 time higher quantum yield than E2 and EE2 at 254 nm. Therefore, faster
280 photolysis of E1 is expected compared to that of E2 and EE2 at this wavelength. At 365 nm,

281 molar absorption coefficients are not significant for the three estrogens and to the best of our
 282 knowledge, their quantum yields at this wavelength were not reported in the literature.

283 Table 7 depicts the first order rate constants of E1, E2 and EE2 in the pilot (experimental data
 284 in the form of C/C_0 curves can be seen in Figure SM3 and Figure SM4 for UVA and UVC
 285 respectively). First of all, the estrogens were photolysed under UVA radiation despite very
 286 low molar absorption coefficients. Constants are of the same order of magnitude for the three
 287 estrogens, ranging from 8.4×10^{-6} to $1.9 \times 10^{-5} \text{ cm}^2 \text{ mJ}^{-1}$ for E1 and EE2 respectively. They
 288 reflect very slow photolysis and less than 2% of the initial concentrations are degraded at
 289 1000 mJ.cm^2 , the maximum relevant UV fluence in AOPs [32], corresponding to 41 min in
 290 the pilot. Then, higher photolysis rates of the three estrogens were observed under UVC
 291 radiation. E2 and EE2 photolysis are 3 to 4 times faster and that of E1 is 113 times faster. As
 292 seen previously, faster photolysis of E1 under UVC radiation was expected given its higher
 293 $\epsilon_{254\text{nm}}$ and $\Phi_{254\text{nm}}$ values. Nevertheless, the photolysis remains slow under UVC radiation with
 294 only 3 to 4% degradation for E2 and EE2 at 1000 mJ cm^2 , whereas E1 was degraded by 62%.
 295 If photolysis may take part in the global degradation of estrogens during AOPs, UV
 296 irradiation cannot be considered as an effective treatment, whether it is under UVA or UVC
 297 radiation.

298 Table 7. Photolysis of E1, E2 and EE2 in the system: k'_p and E_{EO} values.

		E1	E2	EE2
k'_p ($\text{cm}^2 \text{ mJ}^{-1}$)	UVA	$8.4 \pm 3.0 \times 10^{-6}$	$1.2 \pm 0.2 \times 10^{-5}$	$1.9 \pm 0.1 \times 10^{-5}$
	UVC	$9.6 \pm 0.5 \times 10^{-4}$	$4.8 \pm 0.3 \times 10^{-5}$	$6.4 \pm 0.2 \times 10^{-5}$
E_{EO} ($\text{kWh m}^{-3} \text{ order}^{-1}$)	UVA	424.8	223.5	145.9
	UVC	2.1	47.1	31.8

299
 300 These considerations are confirmed by the values of E_{EO} reported in Table 7: with UVA, it
 301 takes between one hundred and four hundred kWh to reduce the concentration of each
 302 estrogen in a m^3 of drinking water by an order of magnitude, which far exceeds the energy

303 consumption compatible with economic feasibility. With UVC, lower E_{EO} values are
 304 obtained, of the order of several tens for E2 and EE2, which remains higher than the threshold
 305 value of $10 \text{ kWh m}^{-3} \text{ order}^{-1}$, even if photolysis alone could be economically viable for E1
 306 hormone degradation.

307 *3.2. Estrogen degradation in drinking water in various AOPs*

308 Pseudo-first order rate constants (k') of the estrogens in drinking water were calculated from
 309 experimental data (available as C/C_0 curves in Figure SM3 and Figure SM4 for UVA and
 310 UVC respectively) and are shown Table 8 as well as associated oxidation constants k'_{ox}
 311 calculated as the difference between k' and k'_p (reported in Table 7). The contribution of
 312 oxidation to the global degradation of the targets ($\%_{ox}$) was also calculated and is presented
 313 in Table 8, the complement to 100 corresponding to the contribution of photolysis.

314 Table 8. Pseudo-first order degradation constants (k') of E1, E2 and EE2 in the different processes with the
 315 associated oxidation constants (k'_{ox}) and their degradation rates at 1000 mj.cm^{-2} .

Radiation type	Oxidant precursor	Estrogen	Rate constants ($\text{cm}^2 \text{ mJ}^{-1}$)		$\%_{ox}$	Degradation at 1000 mJ cm^{-2} (%)
			k'	k'_{ox}		
UVA	H_2O_2	E1	2.2×10^{-5}	1.4×10^{-5}	64	2.2
		E2	3.3×10^{-5}	2.0×10^{-5}	61	3.2
		EE2	3.5×10^{-5}	1.6×10^{-5}	46	3.4
	$\text{S}_2\text{O}_8^{2-}$	E1	2.1×10^{-4}	2.1×10^{-4}	100	19
		E2	2.8×10^{-4}	2.7×10^{-4}	96	24
		EE2	3.0×10^{-4}	2.8×10^{-4}	93	26
UVC	H_2O_2	E1	1.7×10^{-3}	7.2×10^{-4}	42	81
		E2	9.4×10^{-4}	8.9×10^{-4}	95	61
		EE2	9.5×10^{-4}	8.9×10^{-4}	94	61
	$\text{S}_2\text{O}_8^{2-}$	E1	1.1×10^{-2}	1.0×10^{-2}	91	100
		E2	1.1×10^{-2}	1.1×10^{-2}	100	100
		EE2	1.1×10^{-2}	1.1×10^{-2}	100	100

317 Firstly, as expected, UVC radiation allows for 30 to 80% faster degradation, depending on the
318 oxidant precursor and on the estrogen. k' ranges from $2.2 \pm 0.2 \times 10^{-5}$ to
319 $3.0 \pm 0.2 \times 10^{-4} \text{ cm}^2 \text{ mJ}^{-1}$ under UVA and from $9.4 \pm 0.4 \times 10^{-4}$ to $1.1 \pm 0.1 \times 10^{-3} \text{ cm}^2 \text{ mJ}^{-1}$
320 under UVC radiation. Under UVA radiation, k' are ranked as follows regardless of the
321 oxidant precursor: $E1 < E2 < EE2$. On the other hand, under UVC radiation, k' are similar in
322 the presence of $\text{S}_2\text{O}_8^{2-}$ whereas it is almost twice as high for E1 than for E2 and EE2 in the
323 presence of H_2O_2 .

324 When comparing the oxidant precursors, k' are 7 to 12 times higher with $\text{S}_2\text{O}_8^{2-}$ than with
325 H_2O_2 regardless of the UV type for E2 and EE2 and under UVA only for E1. Under UVC
326 radiation, k'_{E1} is only about 5 times faster with $\text{S}_2\text{O}_8^{2-}$ than with H_2O_2 .

327 In the UVA/ H_2O_2 process, k' goes from $2.2 \pm 0.2 \times 10^{-5}$ to $3.5 \pm 0.3 \times 10^{-5} \text{ cm}^2 \text{ mJ}^{-1}$ with 46
328 to 64% of the degradation achieved by oxidation. These close results are attributed to similar
329 photolysis constants of the estrogens (Table 7) and similar second order rate constants (from
330 1.8 to $2.9 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$) between HO^\cdot and the estrogens [9]. When using $\text{S}_2\text{O}_8^{2-}$, k' values
331 increase by $89 \pm 1\%$ and are similar between the estrogens, ranging from 2.1 to
332 $3.0 \times 10^{-4} \text{ cm}^2 \text{ mJ}^{-1}$, due to close second order rate constants (from 1.8 to $4.1 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$)
333 between $\text{SO}_4^{\cdot-}$ and the estrogens [9]. This increase is attributed to higher k'_{ox} thanks to faster
334 photolysis of $\text{S}_2\text{O}_8^{2-}$ compared to H_2O_2 ($\times 1.2$) (see Table 6). As a consequence, the
335 contribution of oxidation increases, being equal to or greater than 93%.

336 Under UVC radiation, the degradation of the estrogens is accelerated. In the presence of
337 H_2O_2 , k' are from 27 to 77 times higher than those obtained under UVA. In addition to faster
338 estrogen photolysis, H_2O_2 photolysis is 3.5 times faster under UVC than under UVA (Table
339 7). k'_{E2} and k'_{EE2} are similar with a contribution of oxidation reaching 95 and 94%
340 respectively. However, k'_{E1} is almost twice as high as k'_{E2} and k'_{EE2} . It is observed that k'_{ox} are

341 of the same order of magnitude for the three estrogens, from 7.2 to $8.9 \times 10^{-4} \text{ cm}^2 \text{ mJ}^{-1}$.
342 Therefore, faster degradation of E1 is attributed to its high photosensitivity under UVC
343 radiation. Similar trends are observed with the use of $\text{S}_2\text{O}_8^{2-}$: k' are from 39 to 52 times higher
344 under UVC radiation due to faster oxidation. For E2 and EE2, the increase in k'_{ox} is so high
345 that k'_p becomes negligible. Regarding E1, k'_p remains noticeable (about 10% of total
346 degradation). However, a lower k'_{ox} leads to similar k' than that of E2 and EE2. Finally,
347 oxidation plays a major role in E2 and EE2 degradation under UVC regardless of the oxidant
348 precursor whereas the predominant phenomenon in the degradation of E1 varies depending on
349 the oxidant precursor.

350 Estrogen degradation rates at 1000 mJ cm^{-2} are reported in Table 8. With UVC/ $\text{S}_2\text{O}_8^{2-}$, the
351 three estrogens are fully degraded. On the other hand, the UVA/ H_2O_2 process provides less
352 than 4% degradation at 1000 mJ cm^{-2} and does not seem viable. As a consequence, it was not
353 studied in the following parts of the work. Contrasted results are observed with UVA/ $\text{S}_2\text{O}_8^{2-}$
354 (19 to 26% degradation) and UVC/ H_2O_2 (61 to 81% degradation). With the aim of promoting
355 the use of UVA rather than UVC radiation in photoactivated AOPs, coupling UVA radiation
356 to $\text{S}_2\text{O}_8^{2-}$ could be relevant since it induces encouraging results compared to the UVC/ H_2O_2
357 process.

358 The values of E_{EO} calculated for estrogens degradation in drinking water shown in Table 9
359 lead to the same conclusions. Using UVC whatever the free radical precursor seems to be
360 economically feasible with E_{EO} values between 0 and $2 \text{ kWh m}^{-3} \text{ order}^{-1}$. So it seems
361 worthwhile to study the UVC-based AOPs with a complex matrix such as WWTP effluent,
362 even if these conditions may be less favorable. With the UVA/ $\text{S}_2\text{O}_8^{2-}$ process, E_{EO} values are a
363 little bit higher, in the upper range of acceptable values. It is therefore important to determine
364 whether the switch to real matrix leads to a significant increase in E_{EO} values or not. Finally,

365 E_{EO} values obtained with the UVA/H₂O₂ process are around hundred for the three estrogens in
 366 drinking water, so there is no point in going any further with this process.

367 Table 9. Values of E_{EO} for estrogens degradation by photooxidation in different matrices.

Radiation type	Oxidant precursor	Estrogen	E_{EO} (kWh m ⁻³ order ⁻¹)		Ratio $\frac{E_{EO}(DW)}{E_{EO}(WWTP)}$
			Drinking water	WWTP effluent	
UVA	H ₂ O ₂	E1	126.6	-	-
		E2	81.3	-	-
		EE2	84.4	-	-
	S ₂ O ₈ ²⁻	E1	10.3	59.8	5.8
		E2	7.6	55.1	7.2
		EE2	7.3	49.4	6.7
UVC	H ₂ O ₂	E1	1.3	2.1	1.6
		E2	2.2	3.5	1.6
		EE2	2.1	3.2	1.5
	S ₂ O ₈ ²⁻	E1	0.2	0.9	5.0
		E2	0.1	0.9	7.7
		EE2	0.1	0.9	7.1

368

369

370 *3.3. Process comparison in a WWTP effluent*

371 After the study of UV-based AOPs in a simple matrix, it is necessary to implement them in a
 372 real matrix. Real effluents may indeed contain species that absorb UV radiations, react with
 373 radical precursors and/or with free radicals, leading to poorer performance of the process.
 374 Furthermore, it has been shown that photolysis and oxidation are compound dependent. Thus,
 375 it seems interesting to assess the degradation of another kind of micropollutants. This part,
 376 dedicated to the degradation of micropollutants in spiked WWTP effluents, firstly focuses on
 377 the estrogens and then on a mixture of three pharmaceuticals.

378 *3.3.1. Estrogen degradation*

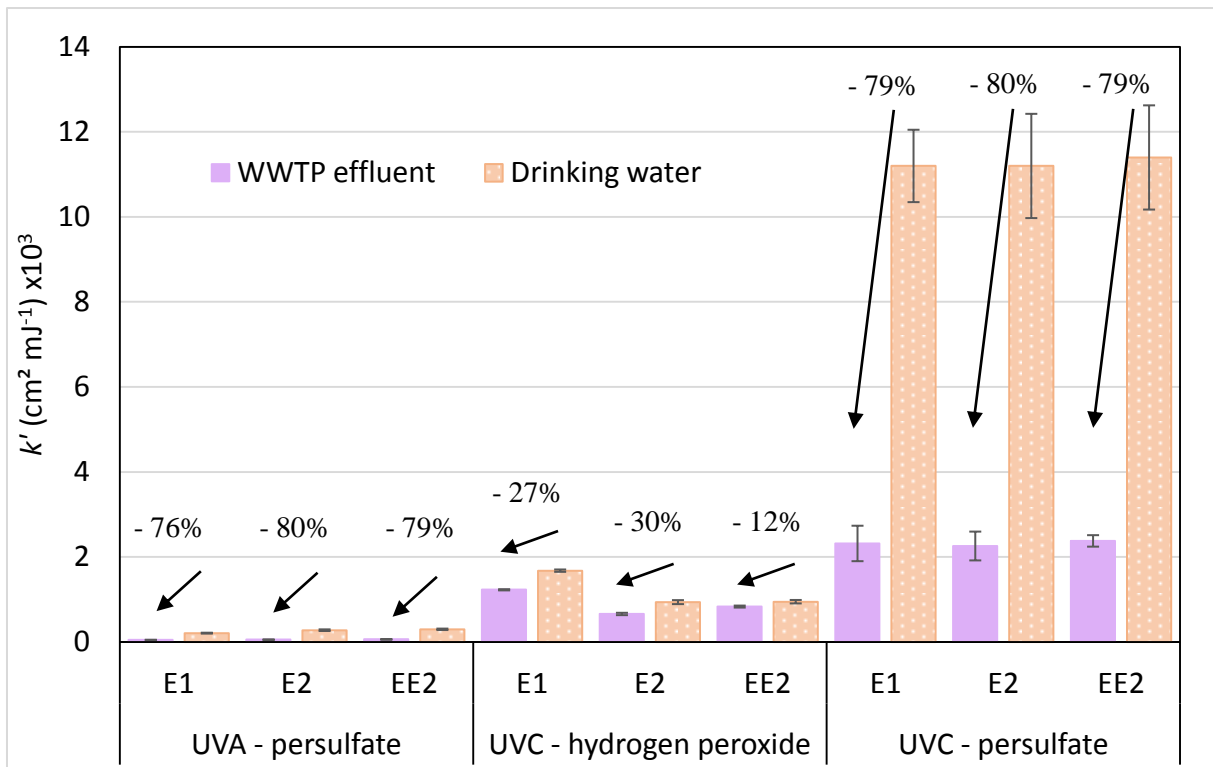
379 WWTP effluent 1 collected at the outlet of a conventional treatment plant (see Table 2 for
 380 more details) and spiked with the three estrogens was used to assess the performance of the
 381 UVA/S₂O₈²⁻, UVC/H₂O₂ and UVC/S₂O₈²⁻ processes (see Table 3 for operating conditions).

382 Pseudo-first order degradation rate constants of the estrogens are presented and compared to
383 those measured in drinking water in Figure 3 (data is available in Table SM2, experimental
384 data is available as C/C_0 curves in Figure SM5).

385 First of all, estrogen degradation rates in WWTP effluent follow the same behaviours as
386 described previously in drinking water: $S_2O_8^{2-}$ induces faster degradation than H_2O_2 and UVC
387 is more efficient than UVA radiation (with $S_2O_8^{2-}$ only since UVA/ H_2O_2 was not
388 implemented). However, k' are lower in the WWTP effluent than in drinking water. Inhibition
389 percentages are presented in Figure 3. They were calculated by comparing the degradation
390 rate constants obtained in the WWTP effluent to those obtained in drinking water. In the
391 presence of $S_2O_8^{2-}$ and regardless of the type of radiation, k' are reduced by 76 to 80%.
392 However, in the UVC/ H_2O_2 process, degradation rates are only inhibited by 27, 30 and 12%
393 for E1, E2 and EE2 respectively. Based on these results, process performances seem to be
394 much more affected in a real matrix when $S_2O_8^{2-}$ is used compared to H_2O_2 .

395 In the literature, the reactivity of H_2O_2 and $S_2O_8^{2-}$ with the WWTP effluent components
396 (mainly organic matter and inorganic anions) was not reported to be significant. The
397 inhibition in a WWTP effluent is rather probably due to the scavenging of the oxidative
398 radicals by the organic matter and inorganic anions such as Cl^- , NO_3^- and HCO_3^- [9, 33, 34].
399 Results obtained in the present study suggest that the scavenging of the radicals by the matrix
400 components is stronger for $SO_4^{\cdot-}$ than for HO^{\cdot} . In both matrices under study, carbonate
401 concentrations are similar. However, the total organic carbon of the effluent is $7.5 \text{ mg}_C \text{ L}^{-1}$
402 whereas that of drinking water is not significant ($< 0.5 \text{ mg}_C \text{ L}^{-1}$). In addition, conductivity,
403 chloride and nitrate concentrations are 2.3, 10 and 4.2 times higher in the WWTP effluent
404 respectively. These differences in matrix composition could indeed induce HO^{\cdot} and $SO_4^{\cdot-}$
405 scavenging. Wang and Wang [35] reported in a literature review that both radicals have
406 similar second order reaction rate constants with HCO_3^- ($9 \times 10^6 \text{ M}^{-1} \text{ s}^{-1}$), that Cl^- have

407 negligible effect and that NO_3^- could have a scavenging impact, although its second order
408 reaction rate with $\text{HO}\cdot$ is not reported and that with $\text{SO}_4\cdot^-$ is negligible
409 ($k''_{\text{SO}_4\cdot^-, \text{NO}_3^-} = 2.1 \text{ M}^{-1} \text{ s}^{-1}$). Therefore, the significant decrease in efficiency of $\text{S}_2\text{O}_8^{2-}$ observed
410 in the present study under both types of radiation could rather be attributed to radical
411 scavenging by organic matter, which would be stronger for $\text{SO}_4\cdot^-$ than for $\text{HO}\cdot$. This
412 inhibition is governed by the competition between the micropollutants of interest and organic
413 matter to react with the radicals. Second order rate constants between the radicals and the
414 organic matter were not determined in the present study. However, Lutze et al. [36] reported
415 higher reaction rates of natural organic matter with $\text{HO}\cdot$ than with $\text{SO}_4\cdot^-$ but they only
416 considered humic acids whereas it was previously reported in the literature that the
417 composition of organic matter in WWTP effluents has a large variation range which also
418 includes fulvic acids, hydrophilic acids, bases and neutral or hydrophobic neutrals for
419 example [37, 38, 39]. Regarding the reactivity between the estrogens and the radicals, Gabet
420 et al. [9] previously reported that second order rate constants are lower with $\text{SO}_4\cdot^-$ (from $1.8 \times$
421 10^9 to $4.1 \times 10^9 \text{ M}^{-1} \text{ s}^{-1}$) than with $\text{HO}\cdot$ (from 1.8×10^{10} to $2.9 \times 10^{10} \text{ M}^{-1} \text{ s}^{-1}$). As a
422 consequence, $\text{SO}_4\cdot^-$ is more likely to be scavenged by organic matter than $\text{HO}\cdot$, depending on
423 their second order reaction rates with the organic matter involved.



424

425 Figure 3. Pseudo-first order degradation rate constants of E1, E2 and EE2 (5 μM) in a WWTP effluent compared to those in drinking water, H_2O_2 or $\text{S}_2\text{O}_8^{2-} = 1 \text{ mM}$.
426

427 In drinking water, $\text{UVA}/\text{S}_2\text{O}_8^{2-}$ seemed to have potential in degrading estrogens: it induced
428 degradation rates only 3 to 8 times slower than $\text{UVC}/\text{H}_2\text{O}_2$. In the WWTP effluent, this is no
429 longer the case because $\text{UVA}/\text{S}_2\text{O}_8^{2-}$ provides 12 to 24 times lower k' values than $\text{UVC}/\text{H}_2\text{O}_2$.

430 Regarding UVC-based processes, $\text{UVC}/\text{S}_2\text{O}_8^{2-}$ was by far the most competitive process in
431 drinking water with 7 to 12 times faster degradations than with H_2O_2 . In a WWTP effluent,
432 they are only 2 to 3.4 times faster than with H_2O_2 . Therefore, even if $\text{UVC}/\text{S}_2\text{O}_8^{2-}$ still gives
433 the best results, performance indicators become of the same order of magnitude as those
434 obtained with $\text{UVC}/\text{H}_2\text{O}_2$.

435 Unsurprisingly, the E_{EO} values reported in Table 9 show that the electrical energy required to
436 reduce estrogens concentrations by one order of magnitude increases when aqueous matrix
437 becomes more complex (from drinking water to WWTP effluent). However, UVC-based
438 processes still exhibit E_{EO} values lower than $10 \text{ kWh m}^{-3} \text{ order}^{-1}$ and even lower than 4,
439 attesting to their economic feasibility. Based on E_{EO} , $\text{UVC}/\text{S}_2\text{O}_8^{2-}$ is more attractive than

440 UVC/H₂O₂ with E_{EO} values two to four times lower. Regarding UVA/S₂O₈²⁻ process,
441 switching to a real matrix raises E_{EO} values (up to between 50 and 60 kWh m⁻³ order⁻¹) above
442 the economic feasibility threshold. While this excess is not strictly prohibitive for UVA
443 technologies, it does indicate that UVC-based AOPs are comparatively more economically
444 attractive.

445 For the two processes that use persulfate ions as radical precursors, E_{EO} values increase by a
446 factor of between 5 and 8 as a result of the matrix change, whether with UVA or UVC,
447 whereas this factor is around 1.5 for UVC/H₂O₂. As seen above based on kinetics
448 considerations, the switch to a real matrix also reduces the performance of persulfate based
449 AOPs more than that of H₂O₂ based ones.

450 3.3.2. Pharmaceutical degradation

451 WWTP effluent 2 collected at the outlet of the same conventional treatment plant (see Table 2
452 for more details) was spiked with a mixture of three pharmaceuticals, namely ibuprofen
453 (IBU), naproxen (NAP) and diclofenac (DCF). The UVA/S₂O₈²⁻, UVC/H₂O₂ and UVC/S₂O₈²⁻
454 processes were carried out in the same conditions as previously. Pseudo-first order
455 degradation rates of the mixture of pharmaceuticals are depicted in Figure 4 (data is available
456 in Table SM3 and experimental data is available as C/C₀ curves in Figure SM6).

457 In all the processes, k' are significantly different between the three compounds and their
458 ranking is similar in the three processes: $k'_{IBU} < k'_{NAP} < k'_{DCF}$. k'_{DCF} is 7 and 11 times higher
459 than k'_{IBU} with H₂O₂ and S₂O₈²⁻ respectively and it is 5.5 times greater than k'_{NAP} with
460 H₂O₂. However, it is less than twice k'_{NAP} with S₂O₈²⁻. As observed for the estrogens, both
461 UVC processes provide faster degradation rates than UVA/S₂O₈²⁻ (from 10 to 63 times with
462 H₂O₂ and from 38 to 56 times with S₂O₈²⁻). However, degradation rates are of the same order
463 of magnitude under UVC radiation with the two oxidant precursors. They are only 1.3 and 3.7

464 times faster with $S_2O_8^{2-}$ for DCF and NAP respectively and the degradation of IBU is on the
465 contrary 1.2 times slower with $S_2O_8^{2-}$ than with H_2O_2 .

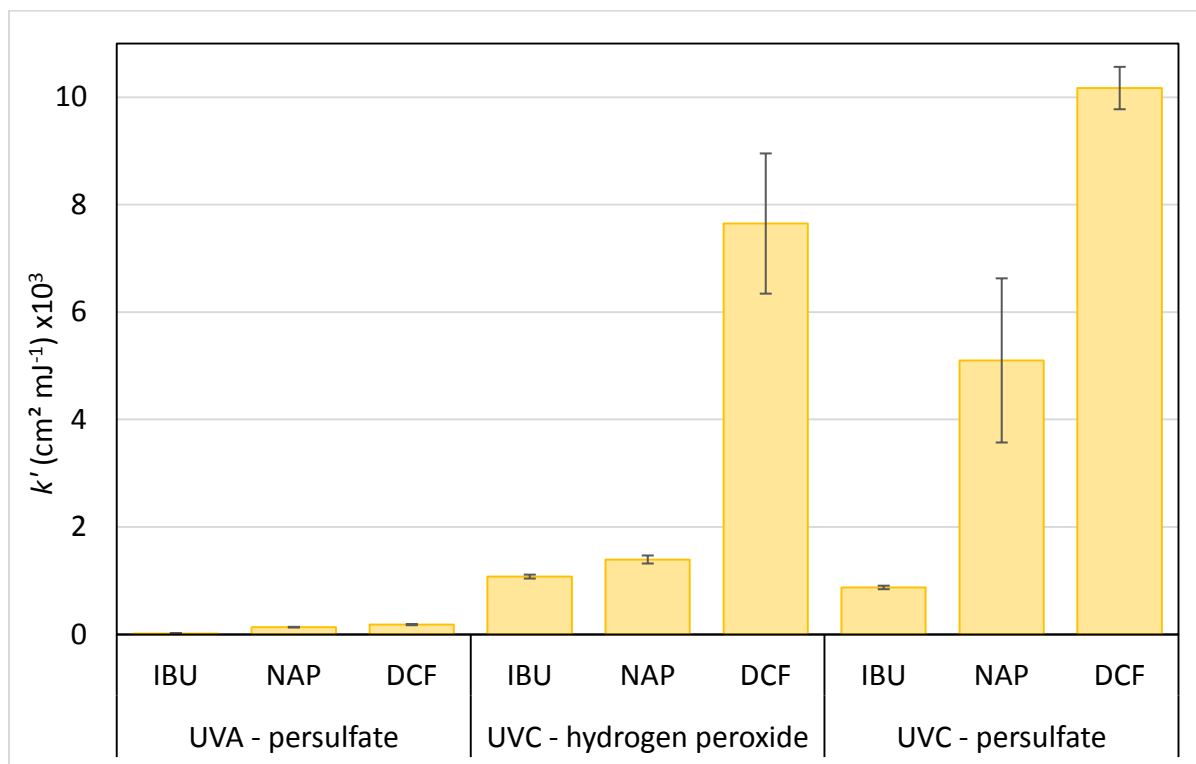
466 Firstly, the difference in degradation rates between the three pharmaceuticals is going to be
467 discussed. Under UVC radiation, DFC is highly photolysable: Fu et al. [40] reported a high
468 photolysis rate of DCF with 92% degradation after 600 s of exposure in their system whereas
469 NAP and IBU were degraded by 52 and 28% respectively. Under UVA radiation, low
470 photolysis is expected in view of the global degradation results reported in Figure 4.
471 However, it has not been studied, to the best of our knowledge. Regarding oxidation, second
472 order rate constants (k'') all are of the same order of magnitude (Table 10). However, they
473 follow the same trend as k' : those of DCF are equal to or higher than those of NAP which are
474 higher than those of IBU. Therefore, the differences in pseudo-first order degradation rates
475 between the pharmaceuticals are attributed to both their different photo-sensitivities and their
476 second order rate constants with $HO\cdot$ and $SO_4\cdot^-$.

477 Table 10. Second order reaction constants between the radicals and IBU, NAP and DCF.

	IBU	NAP	DCF
$k''_{HO\cdot} (M^{-1} s^{-1})$	5.57×10^9 ^[41]	9.05×10^9 ^[42]	9.29×10^9 ^[43]
$k''_{SO_4\cdot^-} (M^{-1} s^{-1})$	1.32×10^9 ^[41]	5.64×10^9 ^[42]	9.2×10^9 ^[44]

478
479 Regarding process efficiency, faster degradation under UVC radiation is attributed to both
480 faster pharmaceutical photolysis and radical generation. Moreover, as seen previously, better
481 degradation in the presence of $S_2O_8^{2-}$ is attributed to the faster generation of $SO_4\cdot^-$ compared
482 to $HO\cdot$. Under UVC radiation, only the degradation of IBU is faster in the presence of H_2O_2
483 than with $S_2O_8^{2-}$. This is due to $k''_{HO\cdot,IBU}$ which is more than 4 times higher than $k''_{SO_4\cdot^-,IBU}$.
484 The same trend is observed with NAP whose second order rate constant is 1.6 times higher
485 with $HO\cdot$ compared to $SO_4\cdot^-$. However, the competition between the different species or the

486 faster generation of $\text{SO}_4^{\cdot-}$ allows NAP to be degraded faster in the UVC/ $\text{S}_2\text{O}_8^{2-}$ process
 487 compared to UVC/ H_2O_2 .



488
 489 Figure 4. Pseudo-first order degradation rate constants of IBU, NAP and DCF (5 μM) in a WWTP effluent, H_2O_2
 490 or $\text{S}_2\text{O}_8^{2-} = 1 \text{ mM}$.

491 E_{EO} calculated for the degradation of pharmaceuticals are shown in Table 11. As already seen
 492 with estrogens, UVC-based AOPs exhibit more favorable values of E_{EO} (lower than 10 kWh
 493 $\text{m}^{-3} \text{ order}^{-1}$) than UVA-based one. With persulphate ions as radical precursor and irrespective
 494 of UV radiation energy, the E_{EO} of IBU is significantly higher than that of NAP and DCF,
 495 which are of the same order of magnitude. E_{EO} obtained from UVC/ H_2O_2 experiments are less
 496 contrasted. It is worth noticing that when comparing the highest and the lowest E_{EO} values for
 497 a given AOP, the ratios vary from 7 to 20 in the case of pharmaceuticals attesting a high
 498 degree of variability depending on the molecules, whereas they were much less dispersed,
 499 from 1.4 to 2.0, in the case of hormones which have fairly similar molecular structures.

500 Table 11. Values of E_{EO} for pharmaceuticals degradation by photooxidation in WWTP effluent 2.

Radiation type	Oxidant precursor	Pharmaceutical	E_{EO} (kWh m ⁻³ order ⁻¹)
UVA	S ₂ O ₈ ²⁻	IBU	203.1
		NAP	23.3
		DCF	15.5
UVC	H ₂ O ₂	IBU	2.1
		NAP	1.7
		DCF	0.3
	S ₂ O ₈ ²⁻	IBU	4.0
		NAP	0.5
		DCF	0.2

501

502 *3.3.3. Removal efficiencies at 1000 mJ cm⁻²*

503 Removal efficiencies at 1000 mJ cm⁻² in the three processes are depicted in Table SM2 for
504 estrogens and in Table SM3 for the pharmaceuticals.

505 The UVA/S₂O₈²⁻ process only allowed weak degradation of the model micropollutants. The
506 estrogens were not degraded by more than 6% and the pharmaceuticals by 17%. On the other
507 hand, UVC radiation allowed satisfactory or good removal efficiencies at 1000 mJ cm⁻²,
508 depending on the model micropollutant and the oxidant precursor. In the presence of H₂O₂,
509 the estrogens were degraded from 43 to 71% and IBU, NAP and DCF were degraded by 66,
510 75 and 100% respectively. In the presence of S₂O₈²⁻, the three estrogens underwent better
511 degradation with removal efficiencies reaching 90 ± 1%. NAP also underwent better
512 degradation and was almost completely degraded (99%) and DCF was still completely
513 removed, whereas IBU was only degraded by 58%, which is slightly poorer than the
514 degradation performances allowed by the UVC/H₂O₂ process, due to a lower k' , as discussed
515 in section 3.3.2. As a consequence, the better performances of the UVC/S₂O₈²⁻ are clear for
516 the estrogens and NAP. However, both UVC processes are comparable for the degradation of
517 DCF which is mainly photodegraded and IBU reaches slightly higher degradation in the

518 presence of H₂O₂, depicting the importance of the nature of the target in the process efficiency
519 assessment.

520 In Switzerland, where a regulation regarding the removal of micropollutants in WWTPs is
521 applicable, it imposes 80% removal on a selection of micropollutants over the complete
522 treatment process. In the present study, the UVC/S₂O₈²⁻ process provides alone such
523 degradation for 5 of the 6 studied compounds and although the UVC/H₂O₂ process does not
524 allow such performances, it could significantly increase the overall micropollutant removal in
525 a WWTP when used as a tertiary treatment.

526 **4. Conclusion**

527 The following main conclusions can be drawn from this study about the feasibility of
528 replacing UVC by UVA in AOPs to degrade micropollutant. Firstly, experiments carried out
529 in drinking water as a simplified matrix with a mixture of estrogens showed that UVA is less
530 efficient than UVC in photolyzing both the radical precursors (H₂O₂ or S₂O₈²⁻) and targeted
531 compounds, which results in lower degradation rates as well as poorer performance at a given
532 UV fluence. Based on E_{EO} calculations, UVA/H₂O₂ seems not economically feasible unlike
533 other AOPs.

534 Experiments carried out with estrogens- or pharmaceuticals-spiked WWTP effluents showed
535 that in the presence of a complex matrix, the UVA/S₂O₈²⁻ process is no longer feasible with
536 values of E_{EO} higher than threshold value. For all AOPs, performance decreases drastically in
537 WWTP matrix, but the UVC-based processes remain economically feasible with satisfactory
538 micropollutant degradation. Persulphate ions still provide better degradation performances
539 than H₂O₂, even though inhibition due to matrix change, expressed as a % relative to drinking
540 water, is stronger, showing a higher scavenging effect of SO₄^{•-} than of HO[•] by organic matter.

541 Since the efficiency of a radical precursor is both compound- and matrix-dependent, further
542 experiments on a larger panel of micropollutants would be required in order to confirm $S_2O_8^{2-}$
543 better efficiency.

544 The E_{EO} is a useful tool to compare AOPs, and especially to compare UVA- and UVC-
545 processes. Nevertheless, it should be completed by another parameter that would enable a fair
546 comparison of radical precursors to be integrated in a technico-economical indicator. For
547 example, the price of a reagent is not the only parameter that induces cost, its implementation
548 has also to be taken into account. However, in view of the experiences carried out in the
549 present study, a more detailed technical and economic approach seems premature.

550 Finally, if the use of mercury-based UVA lamps is ruled out by the results of the present
551 study, there are other UVA radiation sources that could allow for the implementation of less
552 energy consuming processes and for the consideration of UV fluences greater than
553 1000 mJ cm^{-2} (defined for UVC mercury-based lamps). UVA-light emitting diodes (LEDs)
554 are one of them. LEDs have been an emerging light source over the past years and they are
555 known for their high energy efficiency, robustness, clean composition and potential for long
556 lifetimes [45]. UVA-LEDs are particularly interesting because they can be up to 15 times
557 more energy efficient than UVA mercury lamps [46], on the contrary to UVC-LEDs which
558 have low energy efficiency [47]. Another solution for UVA-based processes are solar-driven
559 systems that would allow considering greater energy requirements to reach complete
560 degradation of the targets because solar light is a free and clean energy. However, their major
561 drawback remains process implementation: despite the availability of solar light concentrator,
562 designing a system able to provide appropriate UV fluence for the degradation of
563 micropollutants with solar radiation remains nowadays challenging.

564

565 **5. Declaration of Competing Interest**

566 All authors declare no conflict of interest.

567 **Acknowledgements**

568 The authors wish to acknowledge the financial support of the “Région Auvergne-Rhône-
569 Alpes” for their financial support through the “Pack Ambition Recherche”. This work was
570 performed within the framework of the EUR H2O’Lyon (ANR-17-EURE-0018) of Université
571 de Lyon (UdL), within the program "Investissements d'Avenir” operated by the French
572 National Research Agency (ANR). This work was also supported by the “Federation des
573 Recherches en Environnement” through the CPER “Environnement” founded by the “Région
574 Auvergne,” the French government and FEDER from European community.

575 **References**

- 576 [1] Gallé, T., Pittois, D., Bayerle, M., & Braun, C. (2019). An immission perspective of
577 emerging micropollutant pressure in Luxembourgish surface waters : A simple evaluation
578 scheme for wastewater impact assessment. *Environmental Pollution*, 253, 992- 999.
579 <https://doi.org/10.1016/j.envpol.2019.07.080>.
- 580 [2] Luo, Y., Guo, W., Ngo, H. H., Nghiem, L. D., Hai, F. I., Zhang, J., Liang, S., & Wang, X.
581 C. (2014). A review on the occurrence of micropollutants in the aquatic environment and their
582 fate and removal during wastewater treatment. *Science of The Total Environment*, 473- 474,
583 619- 641. <https://doi.org/10.1016/j.scitotenv.2013.12.065>.
- 584 [3] Pasquini, L., Munoz, J.-F., Pons, M.-N., Yvon, J., Dauchy, X., France, X., Le, N. D.,
585 France-Lanord, C., & Görner, T. (2014). Occurrence of eight household micropollutants in
586 urban wastewater and their fate in a wastewater treatment plant. Statistical evaluation. *Science*
587 *of The Total Environment*, 481, 459- 468. <https://doi.org/10.1016/j.scitotenv.2014.02.075>.
- 588 [4] *Portail assainissement collectif*. (s. d.). Consulté 12 septembre 2022, à l'adresse
589 https://www.assainissement.developpement-durable.gouv.fr/PortailAC/liste_inc_new2
- 590 [5] Cédât, B., de Brauer, C., Métivier, H., Dumont, N., & Tutundjan, R. (2016). Are UV
591 photolysis and UV/H₂O₂ process efficient to treat estrogens in waters? Chemical and
592 biological assessment at pilot scale. *Water Research*, 100, 357- 366.
593 <https://doi.org/10.1016/j.watres.2016.05.040>.
- 594 [6] Chen, P.-J., Rosenfeldt, E. J., Kullman, S. W., Hinton, D. E., & Linden, K. G. (2007).
595 Biological assessments of a mixture of endocrine disruptors at environmentally relevant
596 concentrations in water following UV/H₂O₂ oxidation. *Science of The Total Environment*,
597 376(1- 3), 18- 26. <https://doi.org/10.1016/j.scitotenv.2006.12.051>.

- 598 [7] Song, W., Li, J., Wang, Z., & Zhang, X. (2019). A mini review of activated methods to
599 persulfate-based advanced oxidation process. *Water Science and Technology*, 79(3),
600 573- 579. <https://doi.org/10.2166/wcc.2018.168>.
- 601 [8] Zhang, W., Zhou, S., Sun, J., Meng, X., Luo, J., Zhou, D., & Crittenden, J. (2018). Impact
602 of Chloride Ions on UV/H₂O₂ and UV/Persulfate Advanced Oxidation Processes.
603 *Environmental Science & Technology*, 52(13), 7380- 7389.
604 <https://doi.org/10.1021/acs.est.8b01662>.
- 605 [9] Gabet, A., Métivier, H., de Brauer, C., Mailhot, G., & Brigante, M. (2021). Hydrogen
606 peroxide and persulfate activation using UVA-UVB radiation : Degradation of estrogenic
607 compounds and application in sewage treatment plant waters. *Journal of Hazardous*
608 *Materials*, 405, 124693. <https://doi.org/10.1016/j.jhazmat.2020.124693>.
- 609 [10] Moreira, N. F. F., Narciso-da-Rocha, C., Polo-López, M. I., Pastrana-Martínez, L. M.,
610 Faria, J. L., Manaia, C. M., Fernández-Ibáñez, P., Nunes, O. C., & Silva, A. M. T. (2018).
611 Solar treatment (H₂O₂, TiO₂-P25 and GO-TiO₂ photocatalysis, photo-Fenton) of organic
612 micropollutants, human pathogen indicators, antibiotic resistant bacteria and related genes in
613 urban wastewater. *Water Research*, 135, 195- 206.
614 <https://doi.org/10.1016/j.watres.2018.01.064>.
- 615 [11] Fernandes, C. H. M., Silva, B. F., & Aquino, J. M. (2021). On the performance of distinct
616 electrochemical and solar-based advanced oxidation processes to mineralize the insecticide
617 imidacloprid. *Chemosphere*, 275, 130010.
618 <https://doi.org/10.1016/j.chemosphere.2021.130010>.
- 619 [12] Kowalska, K., Maniakova, G., Carotenuto, M., Sacco, O., Vaiano, V., Lofrano, G., &
620 Rizzo, L. (2020). Removal of carbamazepine, diclofenac and trimethoprim by solar driven
621 advanced oxidation processes in a compound triangular collector based reactor : A

622 comparison between homogeneous and heterogeneous processes. *Chemosphere*, 238, 124665.
623 <https://doi.org/10.1016/j.chemosphere.2019.124665>.

624 [13] Rizzo, L., Lofrano, G., Gago, C., Bredneva, T., Iannece, P., Pazos, M., Krasnogorskaya,
625 N., & Carotenuto, M. (2018). Antibiotic contaminated water treated by photo driven advanced
626 oxidation processes : Ultraviolet/H₂O₂ vs ultraviolet/peracetic acid. *Journal of Cleaner*
627 *Production*, 205, 67- 75. <https://doi.org/10.1016/j.jclepro.2018.09.101>.

628 [14] Velo-Gala, I., Pirán-Montaño, J. A., Rivera-Utrilla, J., Sánchez-Polo, M., & Mota, A. J.
629 (2017). Advanced Oxidation Processes based on the use of UVC and simulated solar radiation
630 to remove the antibiotic tinidazole from water. *Chemical Engineering Journal*, 323, 605- 617.
631 <https://doi.org/10.1016/j.cej.2017.04.102>.

632 [15] Ilyas, H. & van Hullebush, E.D. (2020). Performance comparison of different types of
633 constructed wetlands for the removal of pharmaceuticals and their transformation products: a
634 review. *Environmental Science and Pollution Research*, 27(14): 1-23.
635 <https://doi.org/10.1007/s11356-020-08165-w>.

636 [16] Janex-Habibi, M.-L., Huyard, A., Esperanza, M., & Bruchet, A. (2009). Reduction of
637 endocrine disruptor emissions in the environment : The benefit of wastewater treatment.
638 *Water Research*, 43(6), 1565- 1576. <https://doi.org/10.1016/j.watres.2008.12.051>.

639 [17] Schilirò, T., Pignata, C., Rovere, R., Fea, E., & Gilli, G. (2009). The endocrine disrupting
640 activity of surface waters and of wastewater treatment plant effluents in relation to
641 chlorination. *Chemosphere*, 75(3), 335- 340.
642 <https://doi.org/10.1016/j.chemosphere.2008.12.028>.

643 [18] Adeel, M., Song, X., Wang, Y., Francis, D., & Yang, Y. (2017). Environmental impact of
644 estrogens on human, animal and plant life : A critical review. *Environment International*, 99,
645 107- 119. <https://doi.org/10.1016/j.envint.2016.12.010>.

- 646 [19] Bolton, J. R., & Stefan, M. I. (2002). Fundamental photochemical approach to the
647 concepts of fluence (UV dose) and electrical energy efficiency in photochemical degradation
648 reactions. *Research on Chemical Intermediates*, 28(7- 9), 857- 870.
649 <https://doi.org/10.1163/15685670260469474>.
- 650 [20] Sharpless, C. M., & Linden, K. G. (2003). Experimental and Model Comparisons of
651 Low- and Medium-Pressure Hg Lamps for the Direct and H₂ O₂ Assisted UV
652 Photodegradation of N -Nitrosodimethylamine in Simulated Drinking Water. *Environmental*
653 *Science & Technology*, 37(9), 1933- 1940. <https://doi.org/10.1021/es025814p>.
- 654 [21] Shu, Z., Singh, A., Klammerth, N., McPhedran, K., Bolton, J. R., Belosevic, M., & Gamal
655 El-Din, M. (2016). Pilot-scale UV/H₂O₂ advanced oxidation process for municipal reuse
656 water : Assessing micropollutant degradation and estrogenic impacts on goldfish (*Carassius*
657 *auratus* L.). *Water Research*, 101, 157- 166. <https://doi.org/10.1016/j.watres.2016.05.079>.
- 658 [22] Bolton, J., Bircher, K., Tumas, W., & Tolman, C. (2001). Figures-of merit for the
659 technical development and application of advanced oxidation processes for both electric and
660 solar driven systems. *Pure Appl. Chem.*, 73(4), 627–637.
661 <https://doi.org/10.1351/pac200173040627>
- 662 [23] Sindelar, H.R., Brown, M.T., & Boyer, T.H. (2014). Evaluating UV/H₂O₂,
663 UV/percarbonate, and UV/perborate for natural organic matter reduction from alternative
664 water sources. *Chemosphere*, 105, 112-118.
665 <https://doi.org/10.1016/j.chemosphere.2013.12.040>.
- 666 [24] Vishnuganth, M.A., Remya, N., Kumar, M., & Selvaraju, N. (2016). Photocatalytic
667 degradation of carbofuran by TiO₂-coated activated carbon: Model for kinetic, electrical
668 energy per order and economic analysis. *Journal of Environmental Management*, 181, 201-
669 207. <https://doi.org/10.1016/j.jenvman.2016.06.016>

670 [25] Andrews, S., Huck, P., Chute, A., Bolton, J., & Anderson, W. (1995). UV oxidation for
671 drinking water – feasibility studies for addressing specific water quality issues. *AWWA*
672 *Annual Conference*, 1881–1898, cited by [23].

673 [26] Hokanson, D. R., Li, K., & Trussell, R. R. (2016). A photolysis coefficient for
674 characterizing the response of aqueous constituents to photolysis. *Frontiers of Environmental*
675 *Science & Engineering*, 10(3), 428- 437. <https://doi.org/10.1007/s11783-015-0780-3>.

676 [27] Herrmann, H. (2007). On the photolysis of simple anions and neutral molecules as
677 sources of O^- / OH , SO_x^- and Cl in aqueous solution. *Phys. Chem. Chem. Phys.*, 9(30),
678 3935- 3964. <https://doi.org/10.1039/B618565G>.

679 [28] Goldstein, S., Aschengrau, D., Diamant, Y., & Rabani, J. (2007). Photolysis of Aqueous
680 H_2O_2 : Quantum Yield and Applications for Polychromatic UV Actinometry in
681 Photoreactors. *Environmental Science & Technology*, 41(21), 7486- 7490.
682 <https://doi.org/10.1021/es071379t>.

683 [29] Mark, G., Schuchmann, M. N., Schuchmann, H.-P., & von Sonntag, C. (1990). The
684 photolysis of potassium peroxodisulphate in aqueous solution in the presence of tert-butanol :
685 A simple actinometer for 254 nm radiation. *Journal of Photochemistry and Photobiology A:*
686 *Chemistry*, 55(2), 157- 168. [https://doi.org/10.1016/1010-6030\(90\)80028-V](https://doi.org/10.1016/1010-6030(90)80028-V).

687 [30] Moreira, F. C., Soler, J., Alpendurada, M. F., Boaventura, R. A. R., Brillas, E., & Vilar,
688 V. J. P. (2016). Tertiary treatment of a municipal wastewater toward pharmaceuticals removal
689 by chemical and electrochemical advanced oxidation processes. *Water Research*, 105,
690 251- 263. <https://doi.org/10.1016/j.watres.2016.08.036>.

691 [31] Huang, F., Gao, F., Li, C., & Campos, L. C. (2022). Photodegradation of free estrogens
692 driven by UV light: Effects of operation mode and water matrix. *Science of The Total*
693 *Environment*, 835, 155515. <https://doi.org/10.1016/j.scitotenv.2022.155515>.

694 [32] Rosenfeldt, E.J. & Linden, K.G. (2004). Degradation of endocrine disrupting chemicals
695 bisphenol A, ethinyl estradiol, and estradiol during UV photolysis and advanced oxidation
696 processes. *Environment Science and technology*, 15;38(20):5476-83.
697 <https://doi.org/10.1021/es035413p>.

698 [33] Ma, J., Yang, Y., Jiang, X., Xie, Z., Li, X., Chen, C., & Chen, H. (2018). Impacts of
699 inorganic anions and natural organic matter on thermally activated persulfate oxidation of
700 BTEX in water. *Chemosphere*, 190, 296- 306.
701 <https://doi.org/10.1016/j.chemosphere.2017.09.148>.

702 [34] Olmez-Hanci, T., Dursun, D., Aydin, E., Arslan-Alaton, I., Girit, B., Mita, L., Diano, N.,
703 Mita, D. G., & Guida, M. (2015). S2O8²⁻/UV-C and H2O2/UV-C treatment of Bisphenol A :
704 Assessment of toxicity, estrogenic activity, degradation products and results in real water.
705 *Chemosphere*, 119, S115- S123. <https://doi.org/10.1016/j.chemosphere.2014.06.020>.

706 [35] Wang, J., & Wang, S. (2021). Effect of inorganic anions on the performance of advanced
707 oxidation processes for degradation of organic contaminants. *Chemical Engineering Journal*,
708 411, 128392. <https://doi.org/10.1016/j.cej.2020.128392>.

709 [36] Lutze, H. V., Bircher, S., Rapp, I., Kerlin, N., Bakkour, R., Geisler, M., von Sonntag, C.,
710 & Schmidt, T. C. (2015). Degradation of Chlorotriazine Pesticides by Sulfate Radicals and the
711 Influence of Organic Matter. *Environmental Science & Technology*, 49(3), 1673- 1680.
712 <https://doi.org/10.1021/es503496u>.

713 [37] Imai, A., Fukushima, T., Matsushige, K., Kim, Y.-H., & Choi, K. (2002).
714 Characterization of dissolved organic matter in effluents from wastewater treatment plants.
715 *Water Research*, 36(4), 859- 870. [https://doi.org/10.1016/S0043-1354\(01\)00283-4](https://doi.org/10.1016/S0043-1354(01)00283-4).

716 [38] Ma, H., Allen, H. E., & Yin, Y. (2001). Characterization of isolated fractions of
717 dissolved organic matter from natural waters and a wastewater effluent. *Water Research*,
718 35(4), 985- 996. [https://doi.org/10.1016/S0043-1354\(00\)00350-X](https://doi.org/10.1016/S0043-1354(00)00350-X).

- 719 [39] Yu, J., Lv, L., Lan, P., Zhang, S., Pan, B., & Zhang, W. (2012). Effect of effluent organic
720 matter on the adsorption of perfluorinated compounds onto activated carbon. *Journal of*
721 *Hazardous Materials*, 225- 226, 99- 106. <https://doi.org/10.1016/j.jhazmat.2012.04.073>.
- 722 [40] Fu, Y., Gao, X., Geng, J., Li, S., Wu, G., & Ren, H. (2019). Degradation of three
723 nonsteroidal anti-inflammatory drugs by UV/persulfate : Degradation mechanisms, efficiency
724 in effluents disposal. *Chemical Engineering Journal*, 356, 1032- 1041.
725 <https://doi.org/10.1016/j.cej.2018.08.013>.
- 726 [41] Kwon, M., Kim, S., Yoon, Y., Jung, Y., Hwang, T.-M., Lee, J., & Kang, J.-W. (2015).
727 Comparative evaluation of ibuprofen removal by UV/H₂O₂ and UV/S₂O₈²⁻ processes for
728 wastewater treatment. *Chemical Engineering Journal*, 269, 379- 390.
729 <https://doi.org/10.1016/j.cej.2015.01.125>.
- 730 [42] Dong, S., Zhai, X., Pi, R., Wei, J., Wang, Y., & Sun, X. (2020). Efficient degradation of
731 naproxen by persulfate activated with zero-valent iron : Performance, kinetic and degradation
732 pathways. *Water Science and Technology*, 81(10), 2078- 2091.
733 <https://doi.org/10.2166/wst.2020.263>.
- 734 [43] Yu, H., Nie, E., Xu, J., Yan, S., Cooper, W. J., & Song, W. (2013). Degradation of
735 Diclofenac by Advanced Oxidation and Reduction Processes : Kinetic Studies, Degradation
736 Pathways and Toxicity Assessments. *Water Research*, 47(5), 1909- 1918.
737 <https://doi.org/10.1016/j.watres.2013.01.016>.
- 738 [44] Mahdi Ahmed, M., Barbati, S., Doumenq, P., & Chiron, S. (2012). Sulfate radical anion
739 oxidation of diclofenac and sulfamethoxazole for water decontamination. *Chemical*
740 *Engineering Journal*, 197, 440- 447. <https://doi.org/10.1016/j.cej.2012.05.040>.
- 741 [45] Autin, O., Romelot, C., Rust, L., Hart, J., Jarvis, P., MacAdam, J., Parsons, S. A., &
742 Jefferson, B. (2013). Evaluation of a UV-light emitting diodes unit for the removal of

743 micropollutants in water for low energy advanced oxidation processes. *Chemosphere*, 92(6),
744 745- 751. <https://doi.org/10.1016/j.chemosphere.2013.04.028>.

745 [46] Rodríguez-Chueca, J., Ferreira, L. C., Fernandes, J. R., Tavares, P. B., Lucas, M. S., &
746 Peres, J. A. (2015). Photocatalytic discolouration of Reactive Black 5 by UV-A LEDs and
747 solar radiation. *Journal of Environmental Chemical Engineering*, 3(4), 2948- 2956.
748 <https://doi.org/10.1016/j.jece.2015.10.019>.

749 [47] Matafonova, G., & Batoev, V. (2018). Recent advances in application of UV light-
750 emitting diodes for degrading organic pollutants in water through advanced oxidation
751 processes : A review. *Water Research*, 132, 177- 189.
752 <https://doi.org/10.1016/j.watres.2017.12.079>.

753

754

Supplementary Materials

755 **Pilot-scale assessment of the viability of UVA radiation for H_2O_2 or $\text{S}_2\text{O}_8^{2-}$**

756 **activation in advanced oxidation processes**

757

758 Anaëlle Gabet^{1,2}, Christine de Brauer¹, Gilles Mailhot², Marcello Brigante², H  l  ne M  tivier¹

759 ¹ Univ Lyon, INSA Lyon, DEEP, EA7429, 69621 Villeurbanne, France

760 ² Universit   Clermont Auvergne, CNRS, Clermont Auvergne INP, Institut de Chimie de

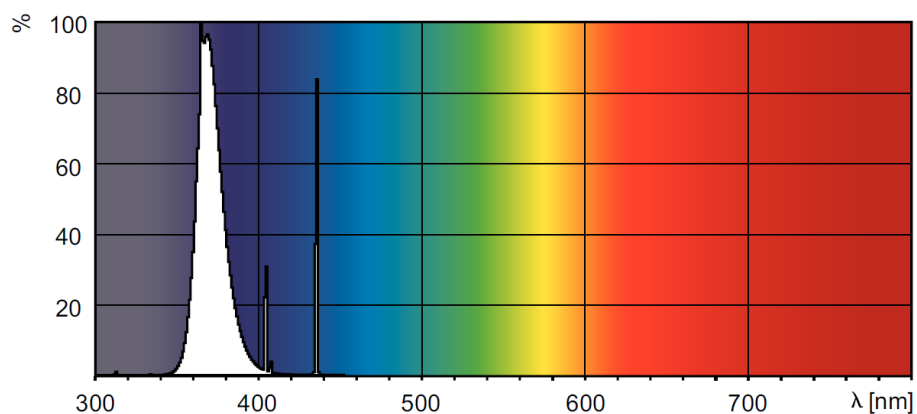
761 Clermont-Ferrand, F-63000 Clermont-Ferrand, France

762 *corresponding author: helene.metivier@insa-lyon.fr

763

764

Figure SM1. UVA lamp emission spectrum (Philips).



765

766

767

768

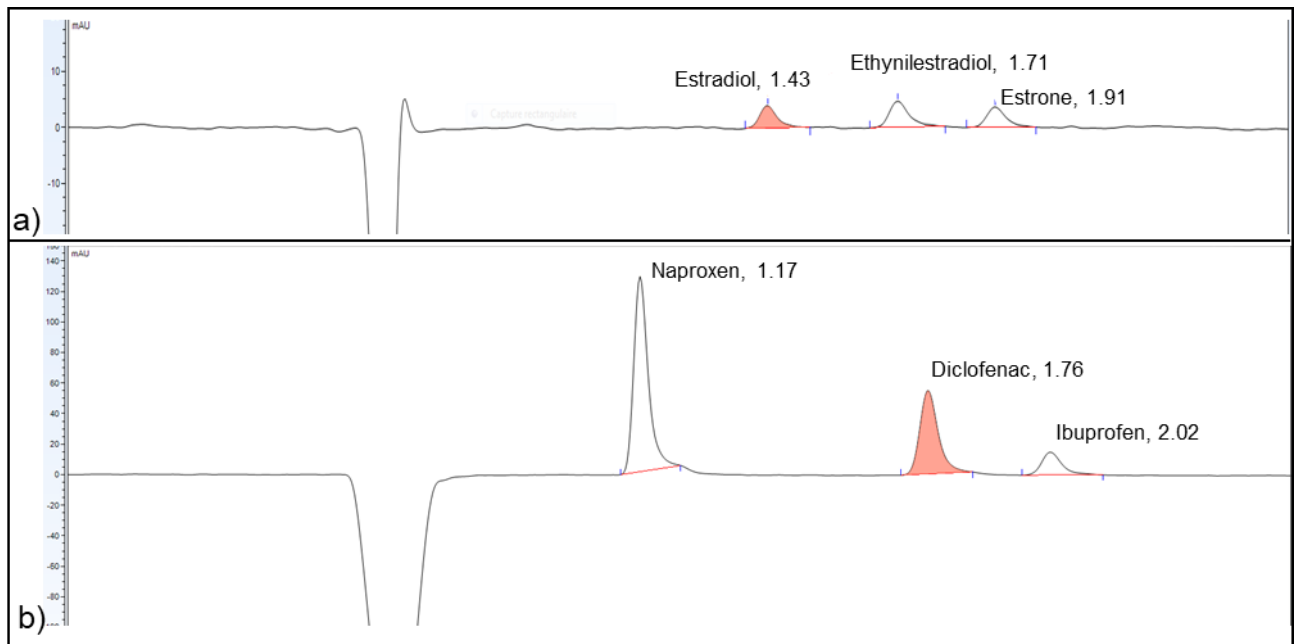
769

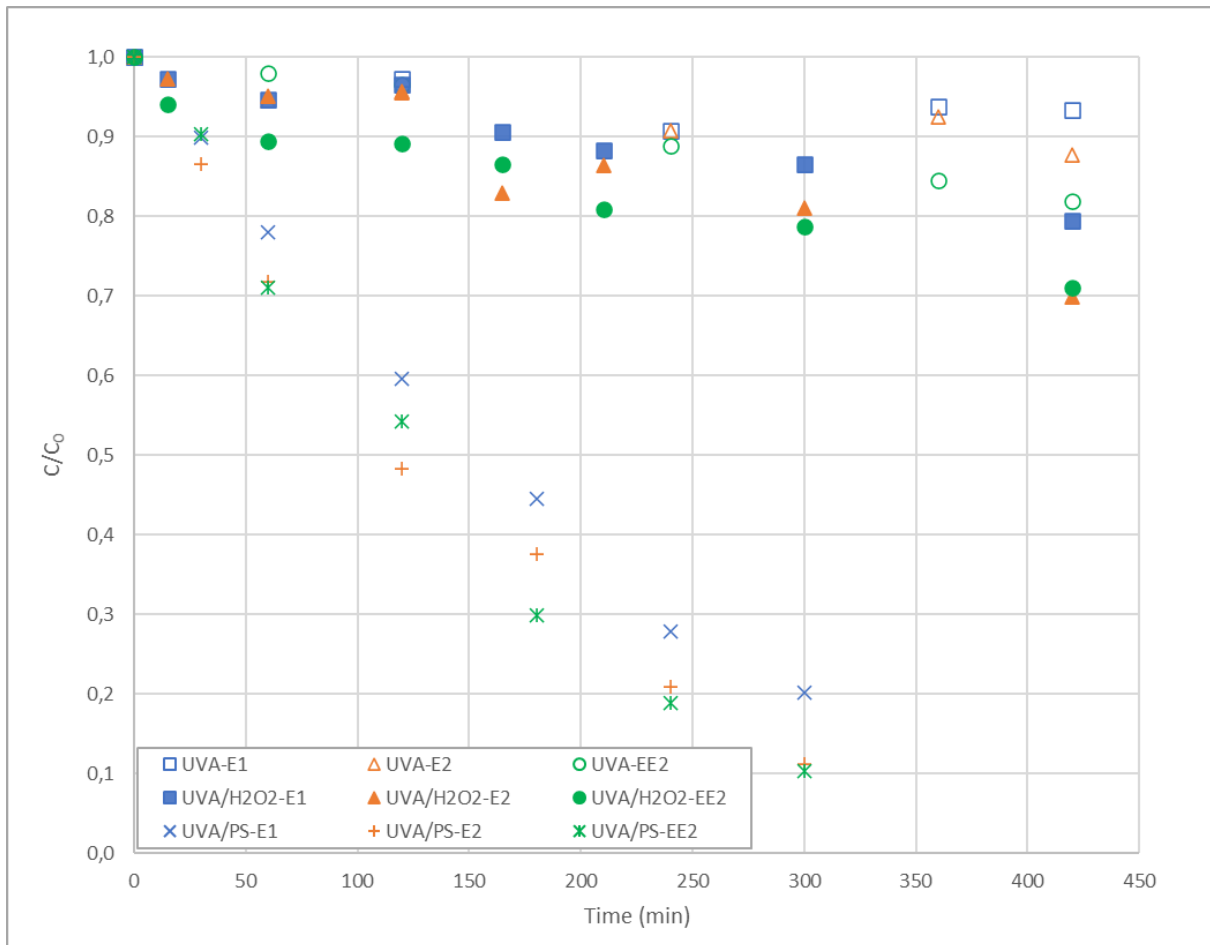
770

771

772

773

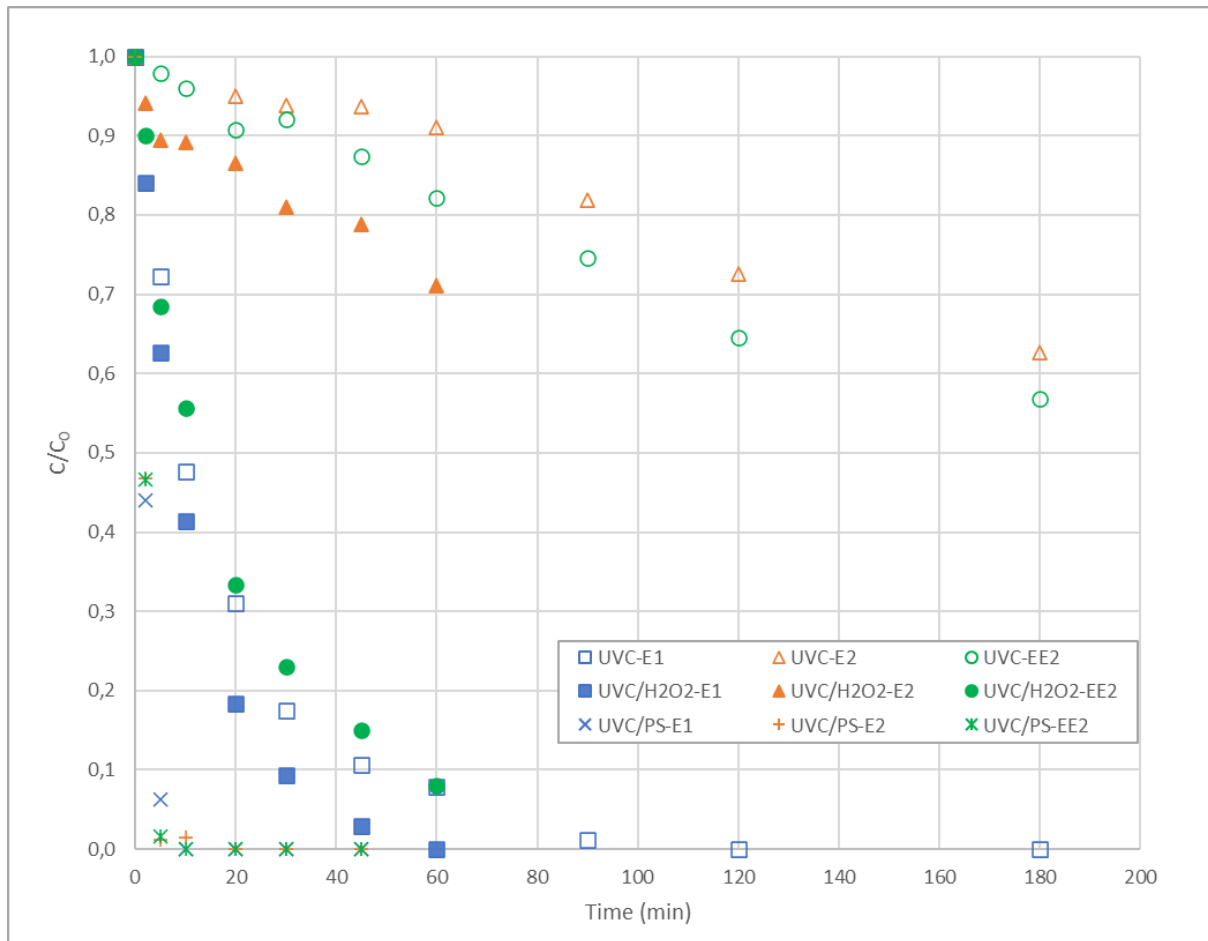




778

779 Initial concentration of estrogens: 5 μM each; initial concentration of radical precursor (hydrogen peroxide (H₂O₂) or
 780 persulphate ions (PS)): 1 mM; aqueous matrix is drinking water (Table 2).

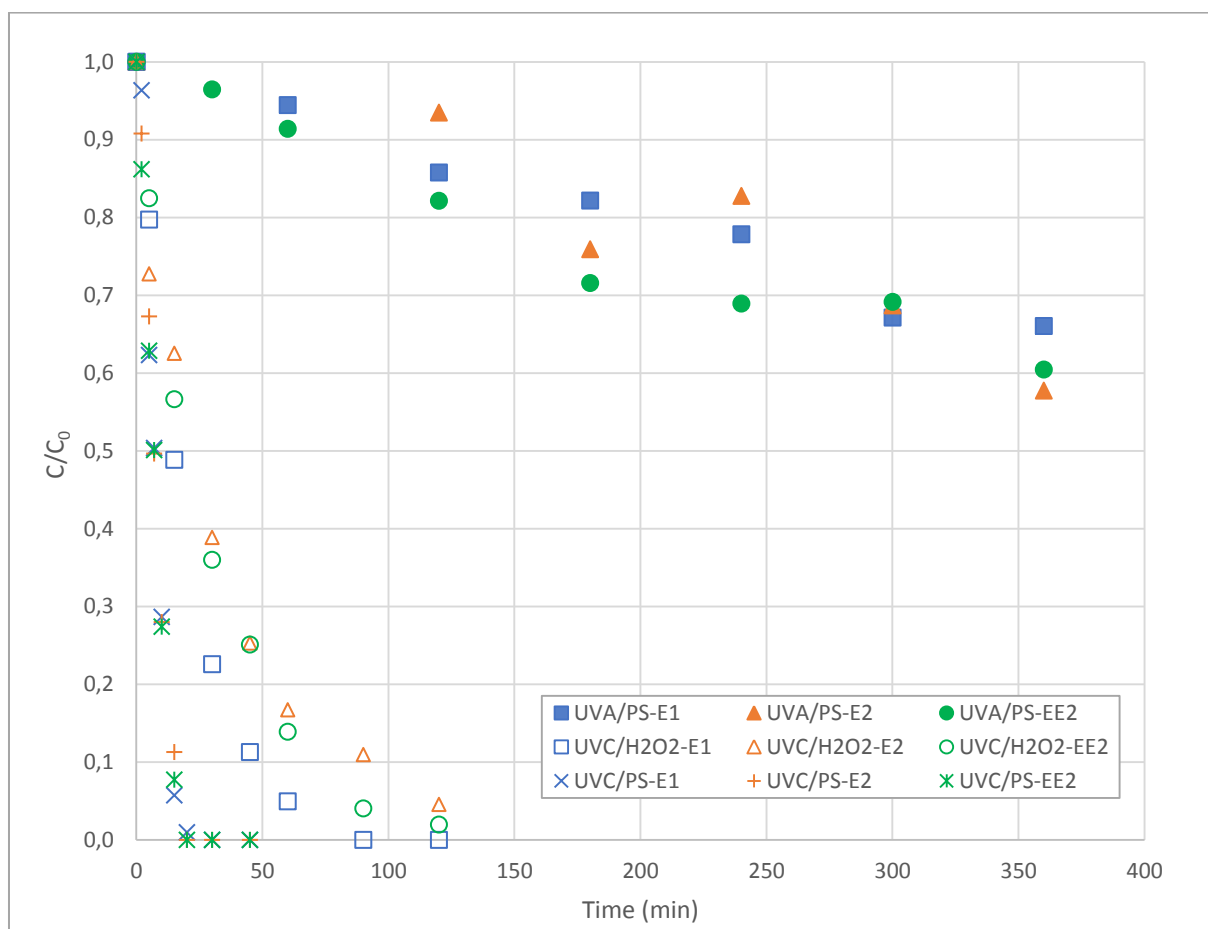
781



783

784 Initial concentration of estrogens: 5 μM each; initial concentration of radical precursor (hydrogen peroxide (H₂O₂) or
 785 persulphate ions (PS)): 1 mM; aqueous matrix is drinking water (Table 2).

786



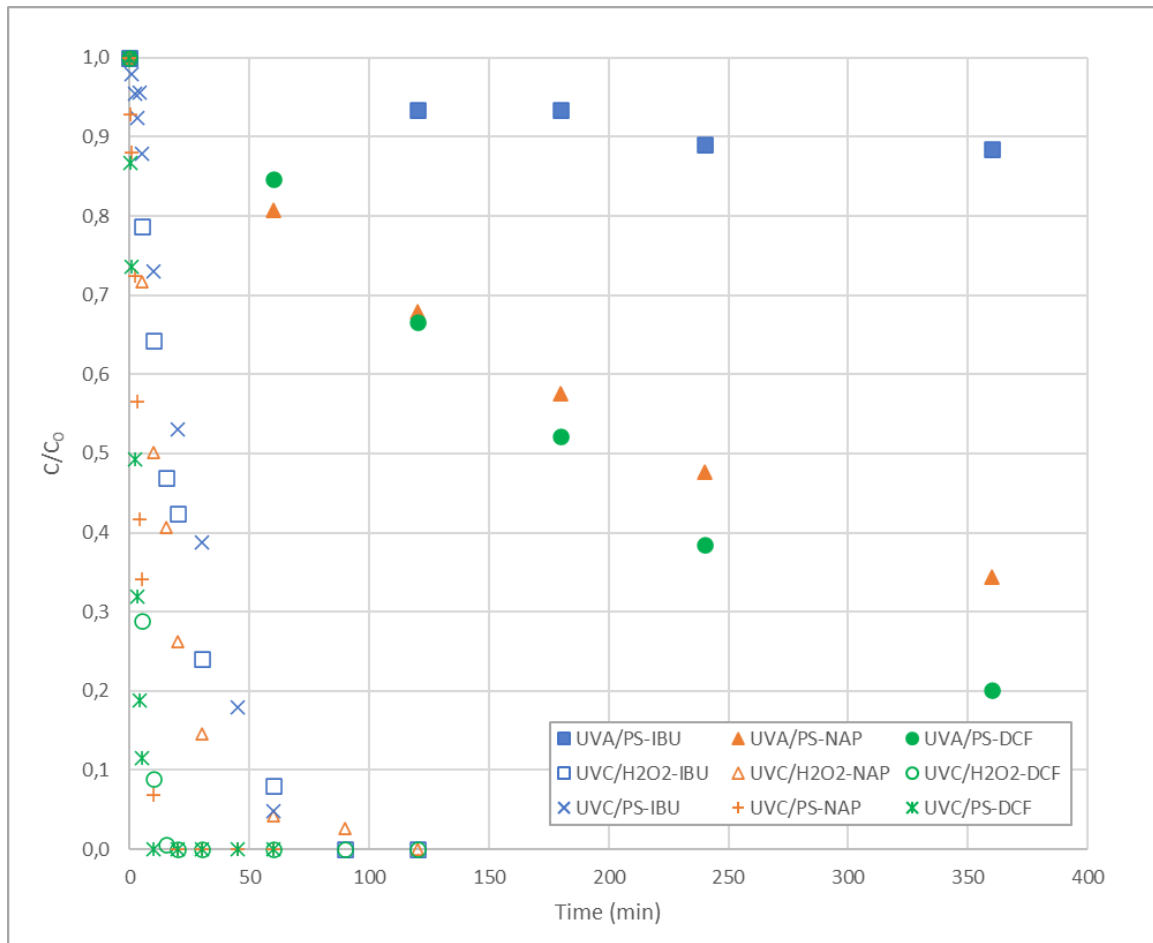
788

789 Initial concentration of estrogens: 5 μM each; initial concentration of radical precursor (hydrogen peroxide (H_2O_2) or
 790 persulphate ions (PS)): 1 mM; aqueous matrix is WWTP effluent 1 (Table 2).

791

792

Figure SM6. AOPs for pharmaceuticals degradation in WWTP effluent.



793

794 Initial concentration of pharmaceuticals: 5 μM each; initial concentration of radical precursor (hydrogen peroxide (H_2O_2) or
 795 persulphate ions (PS)): 1 mM; aqueous matrix is WWTP effluent 2 (Table 2)

796

797

Table SM1. Estimates of E_{EO} for micropollutant reduction by photolysis or different AOPs.

Matrix	Radiation type	Oxidant precursor	Time (min)	Target molecule	C_i (μM)	C_f (μM)	E_{EO} ($\text{kWh m}^{-3} \text{ order}^{-1}$)
Estrogens							
Drinking water	UVA	None	420	E1	4.09	3.82	424.8
				E2	4.60	4.04	223.5
				EE2	4.38	3.59	145.9
	UVC	None	90	E1	4.21	0.05	2.1
				E2	4.29	3.52	47.1
				EE2	4.49	3.35	31.8
	UVA	H_2O_2	420	E1	4.20	3.34	126.6
				E2	4.50	3.15	81.3
				EE2	4.57	3.24	84.4
		$\text{S}_2\text{O}_8^{2-}$	240	E1	4.32	0.87	10.3
				E2	4.51	0.51	7.6
				EE2	4.61	0.48	7.3
	UVC	H_2O_2	30	E1	4.72	0.44	1.3
				E2	4.86	1.17	2.2
				EE2	4.75	1.09	2.1
$\text{S}_2\text{O}_8^{2-}$		5	E1	3.99	0.25	0.2	
			E2	4.26	0.06	0.1	
			EE2	5.35	0.09	0.1	
WWTP effluent 1	UVA	$\text{S}_2\text{O}_8^{2-}$	360	E1	4.38	2.89	59.8
				E2	4.38	2.79	55.1
				EE2	4.78	2.89	49.4
	UVC	H_2O_2	60	E1	4.75	0.23	2.1
				E2	4.85	0.81	3.5
				EE2	5.07	0.71	3.2
		$\text{S}_2\text{O}_8^{2-}$	7	E1	4.1	1.89	0.9
				E2	4.34	1.99	0.9
				EE2	4.78	2.14	0.9
Pharmaceuticals							
WWTP effluent 2	UVA	$\text{S}_2\text{O}_8^{2-}$	360	IBU	5.42	4.79	203.1
				NAP	4.71	1.62	23.3
				DCF	4.34	0.87	15.5
	UVC	H_2O_2	15	IBU	5.70	2.67	2.1
				NAP	5.38	2.18	1.7
				DCF	4.70	0.03	0.3
		$\text{S}_2\text{O}_8^{2-}$	5	IBU	5.15	4.53	4.0
				NAP	4.03	1.38	0.5
				DCF	4.03	0.46	0.2

801
802

Table SM2. Pseudo-first order degradation constants of E1, E2 and EE2 in the different processes with two different matrices and the degradation rates at 1000 mJ cm⁻² in WWTP effluent 1.

			Drinking water	WWTP effluent 1	
Radiation type	Oxidant precursor	Estrogen	Rate constants k' (cm ² mJ ⁻¹)		Degradation at 1000 mJ cm ⁻² (%)
UVA	S ₂ O ₈ ²⁻	E1	2.1 × 10 ⁻⁴	5.2 × 10 ⁻⁵	5
		E2	2.8 × 10 ⁻⁴	5.5 × 10 ⁻⁵	5
		EE2	3.0 × 10 ⁻⁴	6.3 × 10 ⁻⁵	6
UVC	H ₂ O ₂	E1	1.7 × 10 ⁻³	1.2 × 10 ⁻³	71
		E2	9.4 × 10 ⁻⁴	6.6 × 10 ⁻⁴	48
		EE2	9.5 × 10 ⁻⁴	8.4 × 10 ⁻⁴	43
	S ₂ O ₈ ²⁻	E1	1.1 × 10 ⁻²	2.3 × 10 ⁻³	90
		E2	1.1 × 10 ⁻²	2.3 × 10 ⁻³	90
		EE2	1.1 × 10 ⁻²	2.4 × 10 ⁻³	91

803

804

805

806
807

Table SM3. Pseudo-first order degradation constants of IBU, NAP and DCF in the different processes with WWTP effluent 2 as a matrix and the degradation rates at 1000 mJ cm⁻².

Radiation type	Oxidant precursor	Pharmaceuticals	Rate constants k' (cm ² mJ ⁻¹)	Degradation at 1000 mJ cm ⁻² (%)
UVA	S ₂ O ₈ ²⁻	IBU	1.7 × 10 ⁻⁵	2
		NAP	1.3 × 10 ⁻⁴	13
		DCF	1.8 × 10 ⁻⁴	17
UVC	H ₂ O ₂	IBU	1.1 × 10 ⁻³	66
		NAP	1.4 × 10 ⁻³	75
		DCF	7.7 × 10 ⁻³	100
	S ₂ O ₈ ²⁻	IBU	8.7 × 10 ⁻⁴	58
		NAP	5.1 × 10 ⁻³	99
		DCF	1.0 × 10 ⁻²	100

808

809