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Magnesium batteries: towards a first use of graphite fluorides

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Abstract

Graphite fluorides obtained by fluorination of graphite at room temperature and after a subsequent re-fluorination treatment were characterised by X-Ray Diffraction and ¹⁹F MAS NMR. Their electrochemical performances as cathode materials in magnesium batteries have been investigated. Four different electrolytes (0.5 or 1 M Mg(ClO₄)₂ in ACN, DMSO, PC and THF) were used for these tests. The specific energy and power densities were estimated for all media. A comparison of the performances between lithium and magnesium batteries was realised. The effect, on the electrochemical performances, of a re-fluorination treatment at 250 °C was also studied.

Keywords:

Graphite Fluoride; Magnesium Batteries; Electrochemical Properties

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1. Introduction

Progress in portable electronic devices requires more and more efficient batteries. Ion-transfer batteries are well adapted for such applications. Up to date, most of the research performed in this field concerns lithium intercalation batteries [1,2]. In answer to the two important problems regarding the cost of such batteries and their environmental impact, magnesium, because of its high natural abundance and lesser harm in comparison with lithium, seems to be a promising alternative for negative electrodes. However, the standard potential of the aqueous Mg^{2+}/Mg redox couple is 0.66 V higher than the one of Li^+/Li (figure 1), which prefigures a lower discharge potential for magnesium batteries, in addition to a lower energy density due to a smaller specific capacity-to-weight ratio for magnesium [3]. A magnesium battery is then a compromise between a high performance system and a lower cost one. Magnesium intercalation has been less studied than lithium intercalation. The following and non exhaustive list gives some examples of materials allowing accommodation of magnesium under ionic form: transition metals oxides (V_2O_5 [4,5], MoO_3 [6], $\text{Mn}_3\text{Co}_2\text{O}_4$ [7], ...), sulphides (TiS_2 [8], NbS_3 [9], $\text{Mg}_x\text{Mo}_3\text{S}_4$ [10], ...), and borides (MoB_2 [8], TiB_2 [8], ...).

Graphite fluorides have already been extensively studied as cathode materials in lithium [11-17] or aluminium batteries [18]. Thus, covalent graphite fluorides yield a discharge capacity of about 900 Ah kg^{-1} associated to a discharge potential close to 2.1 V vs Li^+/Li [11-13]. For aluminium batteries, the discharge potential and capacity are close to 1 V vs Al^{3+}/Al and 500 Ah kg^{-1} [18], respectively. Interestingly, graphite fluorides prepared according to the method developed earlier by Hamwi et al. [19,20], *i.e.* fluorination at room temperature using a catalytic gaseous mixture of F_2 , HF , MF_n ,

where MF_n is IF_5 , BF_3 , WF_6 , ... strongly increases the discharge potential up to 3 V vs Li^+/Li , though a decrease of the capacity is observed concomitantly [14].

Hence, graphite fluorides in association with magnesium may appear as interesting cell-components. In our study, we have investigated, for the first time, the behaviour of graphite fluoride prepared by fluorination of graphite at room temperature, toward magnesium accommodation. The influence of both the electrolyte medium and the thermal post-treatment under fluorine, on the electrochemical performances, was also studied. A comparison with the electrochemical properties observed upon lithium insertion is given.

2. Experimental

2.1. Sample preparation

The starting material was a natural graphite powder from Madagascar with average grain size of about 4 μm . A sample, denoted $CF(IF_5)$, was first prepared according to a room temperature synthesis route using an iodine fluoride (IF_5), hydrogen fluoride (HF) and fluorine (F_2) gaseous mixture, as described in ref [19]. Re-fluorination of the former $CF(IF_5)$ product was carried out under pure F_2 gas at 250 °C, as described in references [21,22], resulting in sample denoted $CF(250)$. According to weight uptake, the following apparent chemical formulae were obtained: $CF_{1.03}$ and $CF_{0.88}$ for $CF(IF_5)$ and $CF(250)$, respectively. As previously shown [21,22] for the raw fluorination product or for re-fluorination temperatures up to 250 °C, part of mass uptake must be assigned to some residual iodine and not to fluorine atoms bonded to

carbon. Hence, the true chemical formulae obtained by chemical analysis were $CF_{0.73}(IF_5)_{0.02}(HF)_{0.06}$ for CF(IF_5) and $CF_{0.76}(IF_5)_{0.01}$ for CF(250).

2.2. Physical characterization

^{19}F Magic Angle Spinning (MAS) Nuclear Magnetic Resonance (NMR) experiments were performed on a Bruker MSL 300 spectrometer (working frequency of 282.2 MHz) with a 4 mm Cross Polarization/Magic Angle Spinning probe from Bruker. The spinning speed employed was 12 kHz. A simple sequence (τ -acquisition) was used with a $\pi/2$ pulse length of 4 μs . All chemical shifts were referenced with respect to $CFCl_3$.

X-ray diffraction (XRD) powder patterns were obtained using a Siemens D501 diffractometer working with the $Cu K_{\alpha}$ radiation.

2.3. Electrochemical study

Typical electrodes were composed of graphite fluoride (about 70 weight %), graphite powder (10%) and carbon black (10%) to ensure electronic conductivity, and polyvinylidene difluoride (PVDF, 10%) as binder. A two electrodes system was used (Swagelok cell type), where magnesium was both reference and counter electrode. A PVDF microporous film, wet with electrolyte, was sandwiched between the composite electrode and a magnesium metal foil. Several electrolytes were tested: 1 M $Mg(ClO_4)_2/ACN$ (acetonitrile), 0.5 M $Mg(ClO_4)_2/DMSO$ (dimethylsulfoxide), 1 M $Mg(ClO_4)_2/PC$ (propylene carbonate) and 1 M $Mg(ClO_4)_2/THF$ (tetrahydrofuran) (+3.33 M H_2O/THF). The electrolyte solvents were doubly distilled prior to use. Perchlorate salts are commercial products (Aldrich). The cells were assembled under argon in a

glove box. Galvanostatic discharges were recorded with a VMP2 - Z from Biologic, at room temperature and under a 10 A kg^{-1} current density.

3. Results and discussion

3.1 Characterization of the graphite fluorides

Preliminary characterisation of all the samples studied was necessary to better understand the behaviour of each material and the electrochemical mechanisms. Figure 2a displays the X-ray diffraction patterns of the two graphite fluoride samples. Four reflections are observed. The first one, at about 14° ($d = 0.631 \text{ nm}$), is typical of the (001) reflection of a first stage fluorine graphite intercalation compound. The second, near 21° (interlayer distance $d = 0.423 \text{ nm}$), corresponds to a residual first stage graphite intercalation compound with IF_z ($z \approx 5$; presence of IF_5 , IF_6^- and IF_7 with IF_5 as main species). The remaining features, at $41\text{-}42^\circ$ ($d=0.220 \text{ nm}$) and 78° ($d=0.123 \text{ nm}$), represent the (100) and (110) reflections issuing from graphite planes, respectively. Accordingly, the repeat distance along the c axis in the $\text{CF}(\text{IF}_5)$ sample is 0.598 nm and the C-C bond length is 0.143 nm , which is typical of sp^2 hybridized carbon atoms. Upon re-fluorination at 250°C , the only structural change is an expansion of the interlayer spacing to 0.638 nm for $\text{CF}(250)$. This fact is explained by a more important F/C ratio in the latter sample.

^{19}F MAS NMR (figure 2b), provides further information about the iodine species content, mainly IF_5 ($\delta_{\text{IF}_5} \approx 2$ and 50 ppm) and IF_6^- ($\delta_{\text{IF}_6^-} \approx 11 \text{ ppm}$), whose variations are

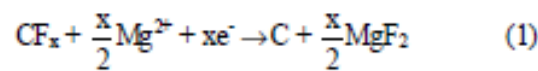
not easily revealed by the X-ray diffraction data. The position of the observed NMR lines also reflects the nature of the C-F bond character.

Inset in figure 2b shows the typical lines (all line intensities normalised to the same value) of the IF_x catalysts over the -20/60 ppm zone. The decrease of the NMR lines area, evidenced by their narrowing is characteristic of a decrease of the iodine content. Moreover, a conversion IF_5 into IF_6^- simultaneously occurs [23]. Over the -200/-100 ppm range, the spectra exhibit a broad band at -160 ppm, attributed to ionocovalent C-F bonds [21-23]. The corresponding line does not seem to be affected by the re-fluorination treatment, but owing to its large width a shift is difficult to detect. However, an Infra-Red study had previously shown [21] that the C-F bond covalency is slightly increased in such conditions.

3.2 Electrochemical properties

3.2.1 Effects of the electrolyte composition and of the re-fluorination treatment

The galvanostatic discharge curves of CF_x , in the different electrolytes (0.5 or 1 M $Mg(ClO_4)_2$ in ACN, DMSO, PC or THF), are shown figure 3. These electrolytes were chosen because they have been commonly used in magnesium batteries. The plateau observed are characteristic of this family of materials [14,24,25] and correspond to the electrochemical insertion of magnesium into graphite fluoride, accompanied by further decomposition into carbon and MgF_2 according to:



The average discharge potentials $E_{1/2}$, measured at half of the maximal capacity, are 1.08, 1.20, 0.73 and 0.72 V for the ACN, DMSO, PC and THF based electrolyte,

respectively. Data on the average discharge potential ($E_{1/2}$), specific capacity (C), specific energy (E_s) and specific power (P_s) are detailed in table 1. The highest $E_{1/2}$ value is obtained in DMSO. This potential is related to the Gibbs free energy of dissociation of the C-F bond, that occurs in the course of reaction 1.

The discrepancy observed regarding the different solvents could be explained by a more or less easy diffusion and/or dissolution of Mg^{2+} from the electrode to the electrolytes. Indeed, the formation of a passivating layer at the surface of a magnesium anode has often been invoked in earlier works dedicated to magnesium batteries [26-30]. The latter is currently recognised as highly impermeable to Mg^{2+} ions, the mobility of the Mg^{2+} ions in the passivating films being extremely low [26-30]. Magnesium dissolution, can then only occur at a high overpotential, via a mechanism involving rupture of the film, as suggested in [27-29]. The dissolution of Mg^{2+} seems then facilitated in the order THF = PC < ACN < DMSO.

One may also infer that the corresponding potential decrease is different for each electrolyte because Mg^{2+} solvation depends on the nature of the solvent. The role played by solvation, may then lie in the respective sizes of the solvation spheres of the cation from one medium to another one. Thus, insertion of Mg^{2+} into the materials is all the more hindered and the resulting potential drop all the more notable as the solvation of Mg^{2+} species is strong. In addition, the potential drop could also result from a partial desolvation occurring at the surface of the host material before intercalation, as suggest in [26].

The theoretical capacity is related to the reduction scheme (1). The transformation of CF_x into carbon and MgF_2 is responsible for the irreversibility of the system. The theoretical maximum capacity is then 756 Ah kg^{-1} for $CF(IF_3)$. However,

the highest experimental capacity obtained is 572 Ah kg^{-1} . The presence of residual iodine fluorides can hinder magnesium penetration into the host lattice and therefore accessibility to the C-F sites, leading to a reduced experimental capacity.

The specific energy density E_s and power density P_s are two important parameters characterising a battery, that can be obtained from the discharge curves (see table 1). As for the capacity and average discharge potential, the most interesting values of the energy and power densities are also obtained in ACN and DMSO electrolytes. For these two solvents, E_s and P_s are of the same order: $E_s = 600\text{-}620 \text{ W kg}^{-1}$ and $P_s = 10\text{-}12 \text{ Wh kg}^{-1}$. For the two other electrolytes, E_s and P_s are divided by a factor close to 2.

A subsequent heat-treatment under fluorine can be used for an enhancement of the C-F bond character [21,22]. From an electrochemical view point, this results in a decrease of the average discharge potential: the higher the covalency, the lower $E_{1/2}$. Thus, a preliminary test was realized in order to verify to which extent this behaviour is followed upon association with a magnesium anode. For $1 \text{ M Mg}(\text{ClO}_4)_2/\text{PC}$, $E_{1/2}$ evolves from 0.73 to 0.68 V after the annealing procedure (figure 4). In parallel, the capacity increases from 400 to 429 Ah kg^{-1} . The re-fluorination treatment yields a higher ratio and therefore a slightly improved capacity. In addition, the weaker content of residual iodine fluorides species, which likely hinder cationic diffusion into the cathodic material, is also an argument in favour of the capacity increase.

3.2.2 Comparison with lithium anodes

Graphite fluorides prepared at high temperature have been used as cathodes in commercial lithium batteries over many years. Therefore, a compound similar to the

present CF(IF₃) sample had been previously studied as a new component likely to enter into such a system [24,25]. It is then interesting to compare the results obtained from lithium and magnesium. The galvanostatic discharge curve of CF(IF₃) used in a lithium battery with 1 M LiClO₄/PC as electrolyte is shown on figure 4. The theoretical optimal capacities are identical for both lithium and magnesium (756 Ah kg⁻¹). This value is however never reached, the capacity obtained upon magnesium accommodation being the lowest. This phenomenon has often been observed in other studies [6,26,31]. The poorer efficiency in the case of magnesium cells may be explained by a more difficult diffusion of Mg²⁺ into the material in comparison with Li⁺. The hindering due to IF₃ species may more strongly reduce the accessibility of magnesium to reactive sites.

The average discharge potential is 1.9 V lower for magnesium in regard to lithium, whereas the theoretical potential drop expected from the difference in the Gibbs free energy of formation of LiF and MgF₂, when put in the Nernst equation ($\Delta E_{1/2} \approx \Delta E^{\circ} = E_{Li}^{\circ} - E_{Mg}^{\circ} = -1/F(\Delta G_{LiF}^{\circ} - 1/2\Delta G_{MgF_2}^{\circ})$), would be 0.6 V. Such a difference is a good indication that a high overpotential takes place, owing to the existence of a passivating layer on the magnesium electrode.

In the case of magnesium batteries, we show that the heat-treatment performed on the fluorinated cathodic material leads to a modification of the electrochemical properties: E_{1/2} diminution (-0.05 V) and capacity increase (7%). A similar behaviour is observed for lithium, *i.e.* a E_{1/2} diminution by -0.16 V accompanied by a simultaneous improvement of the capacity by 10% (figure 4). Both the energy and power values remain unchanged after the fluorination post-treatment for the two kinds of batteries.

Nevertheless, in magnesium-based cells the energy and power densities are reduced by a factor of at least 3 in comparison with lithium systems.

4. Conclusion

In this study, the insertion of Mg^{2+} ions into graphite fluorides has been investigated for the first time. Of the four solvents used, ACN and DMSO based electrolytes give the highest capacity (572 Ah kg^{-1} in the case of ACN) and average discharge potential (1.20 V, for DMSO), yielding consequently the best performances regarding specific energy and power: $\approx 610\text{-}620 \text{ Wh kg}^{-1}$ and $\approx 10\text{-}12 \text{ W kg}^{-1}$, respectively.

The Mg/graphite fluoride system provides reduced overall electrochemical performances in comparison with an equivalent lithium system. Nevertheless, this preliminary approach shows that graphite fluorides could be an interesting alternative for the development of novel magnesium battery technologies. We suggest that serious improvements may be obtained at the cathode level via re-fluorination treatments, whose effects on the electrochemical properties require complementary studies. In parallel, research on the elaboration of an electrolyte which does not quench the electrochemical performances must be performed, the use of solutions of Grignard reagent or solid electrolytes have been evoked. More investigation is needed on both the cathode material and global process before applications can emerge.

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Figure captions

Figure 1:

Electrochemical potentials for X / CF_x batteries (X = Al, Li or Mg). Inset shows the standard potentials (versus SHE electrode) for Li, Mg, Al and F₂.

Figure 2:

(a) X-Ray diffraction patterns of CF(IF₃) and CF(250).

(b) ¹⁹F MAS spectra, at 12 kHz, of CF(IF₃) and CF(250).

Figure 3:

Galvanostatic discharge curves (10 A kg⁻¹, RT) of CF(IF₃) for different electrolytes: (a) 1 M Mg(ClO₄)₂/ACN, (b) 0.5 M Mg(ClO₄)₂/DMSO, (c) 1 M Mg(ClO₄)₂/PC and (d) 1 M Mg(ClO₄)₂/THF (+3.33 M H₂O/THF).

Figure 4:

Galvanostatic discharge curves (10 A kg⁻¹, RT) of CF(IF₃) and CF(250) as lithium cathodes (1 M LiClO₄/PC) and of CF(IF₃) and CF(250) as magnesium cathode (1 M Mg(ClO₄)₂/PC).

Fig.1

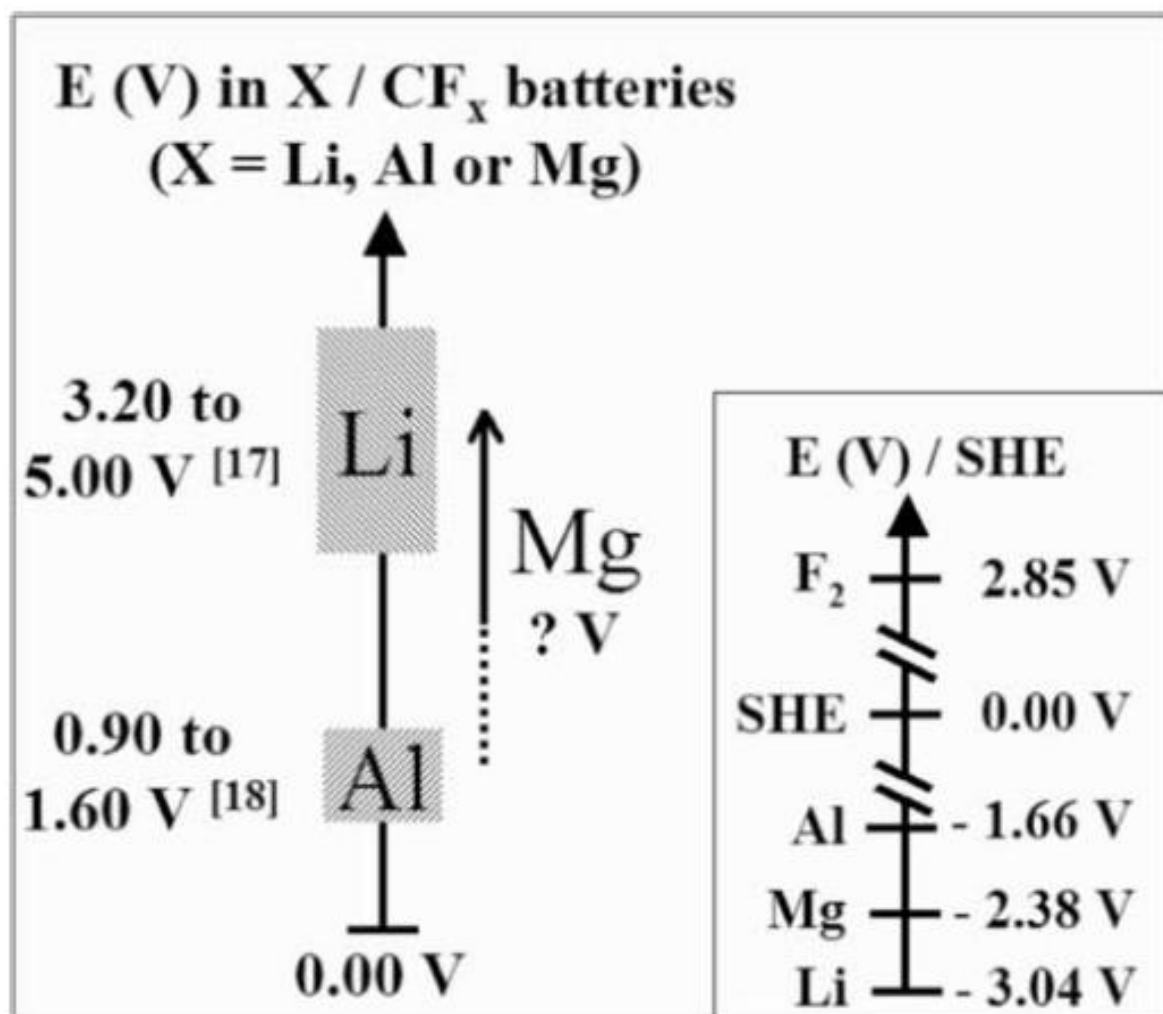


Fig. 2a

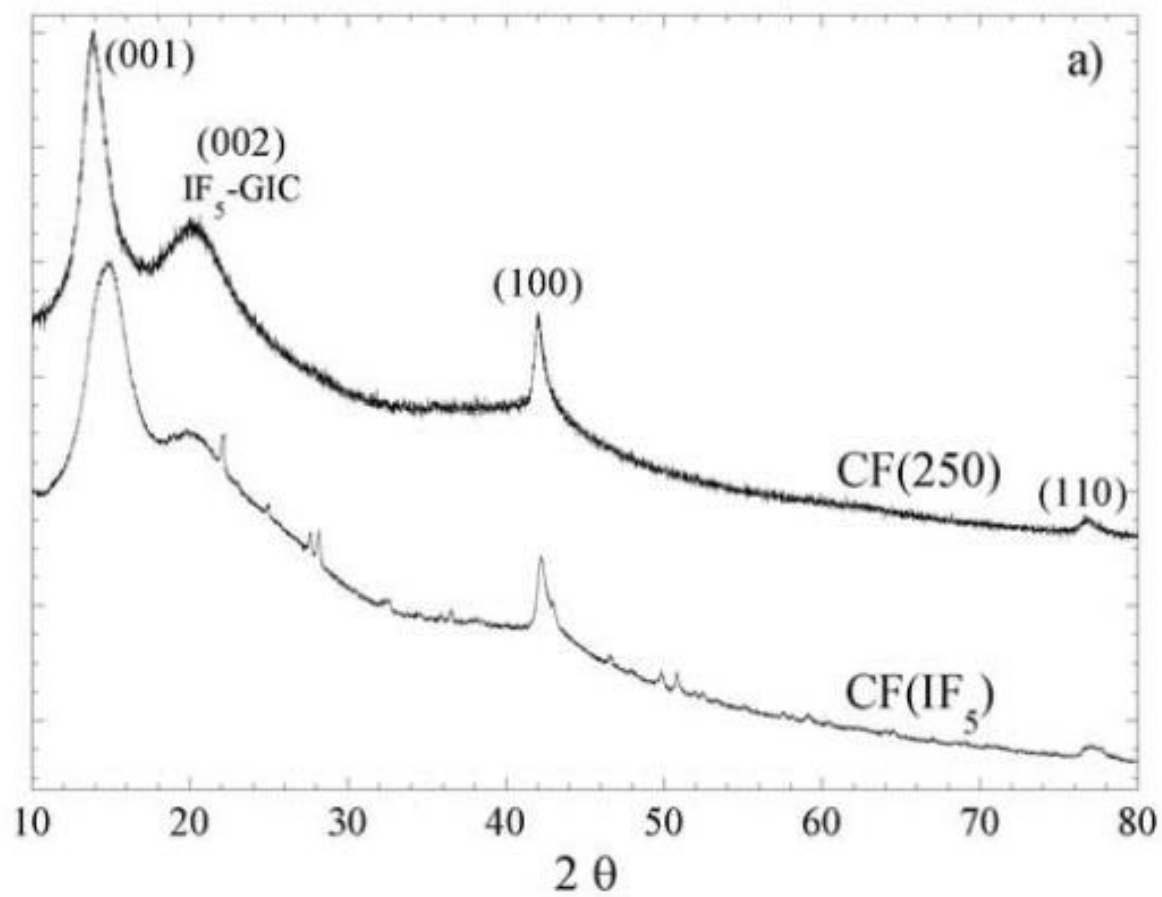


Fig. 2b

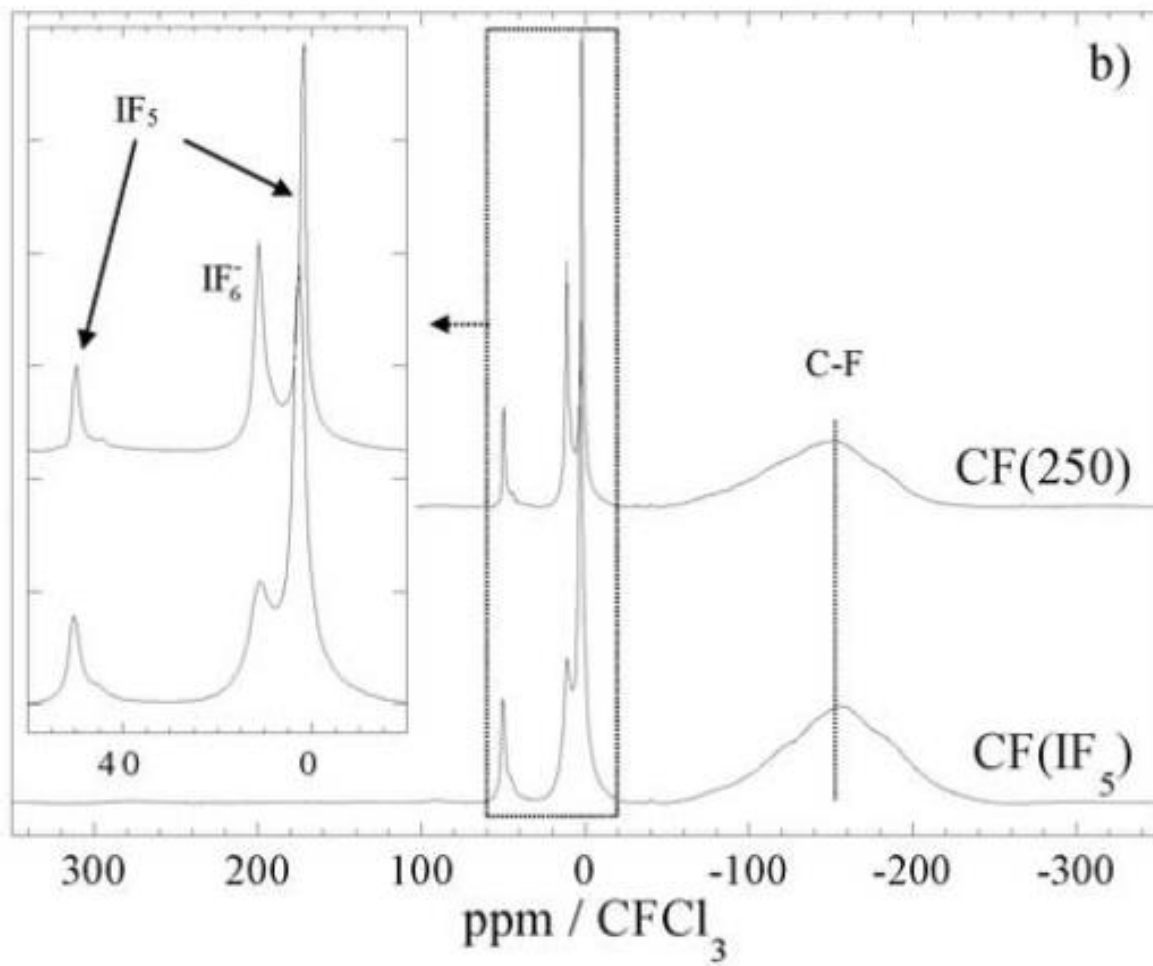


Fig. 3

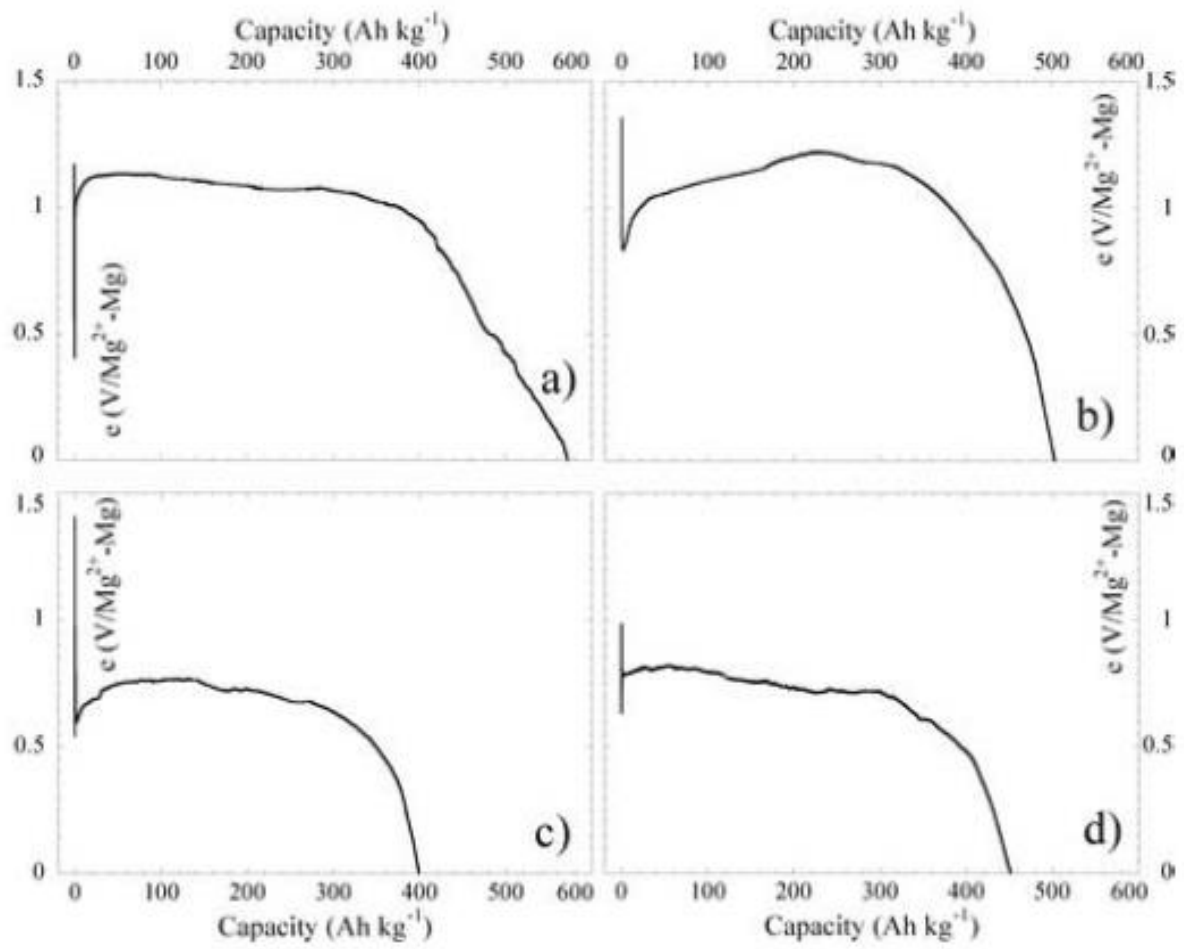


Fig. 4

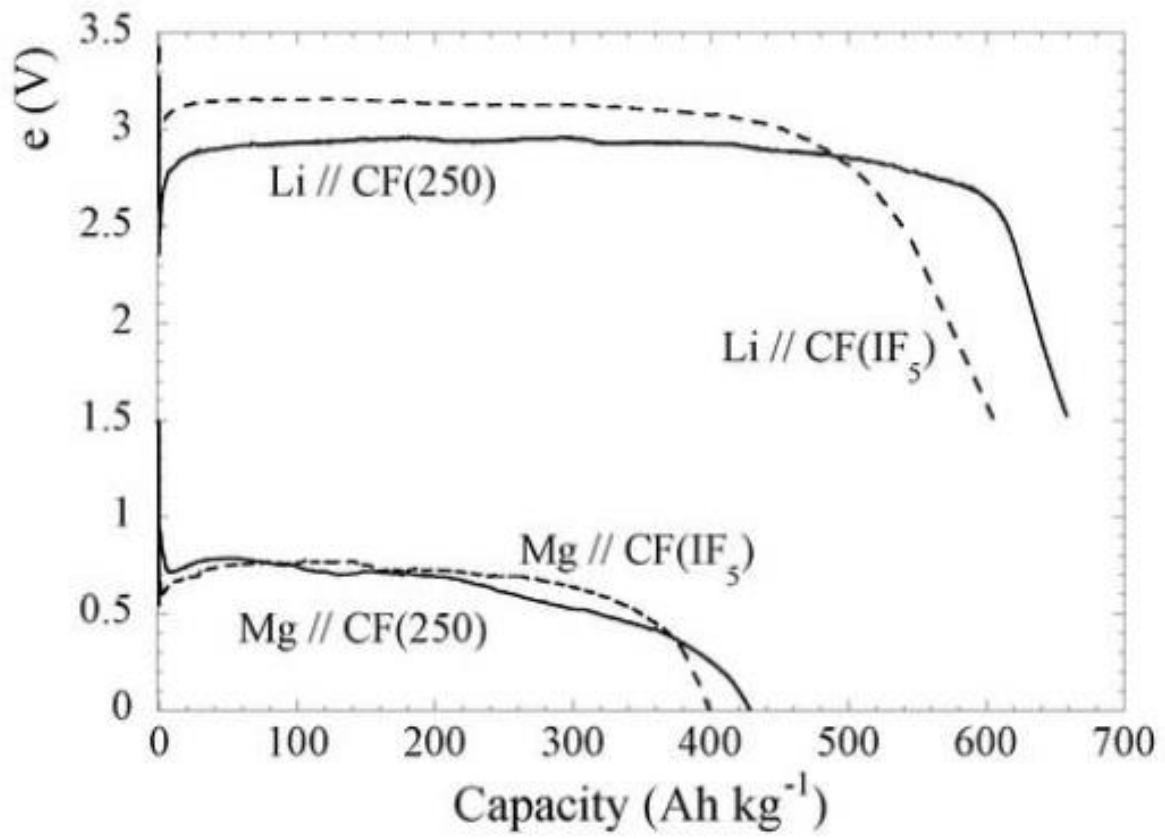


Table 1:

Galvanostatic characteristics of Mg/CF(IF₃) and Mg/CF(250) batteries obtained at room temperature for different electrolytes. $d=10 \text{ A kg}^{-1}$ for all tests.

Sample	Electrolytic solvent	$E_{1/2}$ (V)	Capacity (Ah kg ⁻¹)	Specific energy (Wh kg ⁻¹)	Specific power (W kg ⁻¹)
CF(IF ₃)	ACN	1.08	572	618	10.8
	DMSO	1.20	503	604	12.0
	PC	0.73	400	292	7.30
	THF	0.72	451	325	7.20
CF(250)	PC	0.68	429	292	6.80

$E_s=C \cdot E_{1/2}$ (Wh kg⁻¹) and $P_s=d \cdot E_{1/2}$ (W kg⁻¹). C and d are the discharge capacity (Ah kg⁻¹) and the current density (A kg⁻¹), respectively.