

# Co-adsorption and interaction mechanism of cadmium and sulfamethazine onto activated carbon surface

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1	Co-adsorption and interaction mechanism of cadmium and
2	sulfamethazine onto activated carbon surface
3	
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16	
17	ABSTRACT
18	Owing to their diverse functional groups, antibiotics can easily form complexes with heavy metals; the
19	complexation alters the migration and transformation behavior of both antibiotics and heavy metals. In this
20	study, we investigated the co-adsorption mechanism of sulfamethazine (SMT) and cadmium (Cd <sup>2+</sup> ) heavy
21	metal ions and created an ideal water model containing two major contaminants: sulfamethazine and heavy
22	metal cadmium ions. Combined with the experimental analysis of the interaction mechanism, the results
	1

23	indicate the heterogeneous multilayer adsorption of SMT on the surface of activated carbon (AC). The
24	bridging role of cadmium ions promotes the adsorption of SMT through the formation of SMT-Cd <sup>2+</sup> -AC
25	ternary complexes on the surface of activated carbon. Characterization experiments provided further insight
26	into the adsorption behavior of Cd <sup>2+</sup> and SMT on activated carbon, revealing a strong correlation between
27	the Cd <sup>2+</sup> -SMT complexation and the SMT adsorption capacity. These results indicate that the effects of the
28	coexistence of antibiotics and heavy metal ions should be fully taken into account when investigating the
29	environmental behavior of antibiotics and heavy metal ions.
30	
31	Key words: Heavy Metal, Antibiotics, Bridging, Complexation, Adsorption
32	
33	1. Introduction
34	
35	Fast industrialization and growing social activities result in the composition of wastewater becoming
36	increasingly more complex $[1]$ . The combined pollution by antibiotics and heavy metals, widely affecting
37	actual water systems, is causing widespread concern[ $2, 3$ ]. These two pollutants can cause serious harm to
38	humans and ecosystems $[4]$ . The use of antibacterial agents in the livestock and poultry breeding industry,
39	the land use of livestock and poultry manure, and the centralized treatment of industrial wastewater have led
40	to increasingly serious pollution in surface water or groundwater[5]. Sulfanilamide antibiotics and cadmium
41	heavy metals are the most typical co-pollutants in livestock and poultry breeding industries[6, 7]. Cadmium
42	mainly originates from excessive use of Cd-containing chemicals (insecticides and fungicides) as well as
43	
	cadmium-rich feces[8]. Cadmium fertilizers are employed in domestic poultry breeding[9]. Synthetic

45	foreign antibiotics are usually difficult to be absorbed by animals, and are directly discharged into the
46	receiving waters, where they may pose a serious threat to organisms and trigger antibiotic resistance $[10]$ .
47	Therefore, the efficient removal of antibiotics has attracted worldwide attention $[11]$ . More importantly,
48	antibiotics can form complexes with coexisting metal ions $[11-13]$ , which may significantly alter their
49	chemical properties, migration/transformation process, and ecotoxic reactions [14]. For instance, it has been
50	reported that chelation with antacids (magnesium or aluminum salts) will change the bioavailability of
51	quinolones. Therefore, in environments co-polluted with heavy metal ions, complexation may have
52	unexpected environmental consequences $[\underline{15}]$ .
53	Adsorption methods are the key approaches to study the transfer and transformation of pollutants in
54	the environment. Compared with coagulation, filtration, advanced oxidation, and other methods, the flexible
55	design/operation and low energy consumption of adsorption processes make them the preferred approach for
56	the practical production of clean water from wastewater, with high removal efficiency and less toxic
57	by-products. In addition, this green technology produces no sludge and is compatible with other water
58	treatment systems [16, $17$ ]. Many groups are currently investigating the treatment of antibiotics and heavy
59	metals using adsorption methods. It has been reported that graphene oxide and ordered mesoporous carbon
60	materials with high adsorption capacity can effectively remove ciprofloxacin (CIP) pollutants in water[18]
61	19]. Li et al.[20] prepared a biochar sample that was used to remove tetracycline and sulfadiazine. In
62	addition, many detailed studies have focused on the removal of $Cu^{2+}$ , $Pb^{2+}$ [21], $Hg^{2+}$ [22], $Cr(VI)$ [23], and
63	$Cd^{2+}$ [24] from water using carbon-based materials.
64	The combination of antibiotics and heavy metals has become a new component of polluted water

65 Present research on the adsorption of single heavy metals or antibiotics does not reflect the current state of 66 environmental pollution. Relevant studies have shown that the presence of heavy metals can promote or

67	inhibit the adsorption process of different antibiotics, depending on the type and concentration of heavy
68	metals[25]. Na[26] and co-workers focused on two antibiotics commonly used in aqueous environments
69	(tetracycline hydrochloride and sulfadiazine) and two typical heavy metals (copper and zinc). Their results
70	showed that when antibiotics coexist with heavy metals in water, they can form complexes through
71	complexation. The cations of multivalent heavy metals can significantly enhance the adsorption of
72	antibiotics through the bridging effect [ $27-29$ ]. For example, Cu(II) can improve the adsorption capacity.
73	The formation of CIP-Cu(II) complexes at pH values above 6.0 was simulated by surface complexation on
74	goethite[27]. The presence of Ni(II) promoted the adsorption of CIP on activated carbon (AC)[29]. The
75	mechanism by which metal ion complexation affects antibiotic adsorption is extremely complex. Although
76	some reports on the co-adsorption behavior of composite antibiotics and metal pollutants are available,
77	studies on the influence of metal ions on the adsorption of antibiotics are still scarce. In particular, the
78	mechanism of co-adsorption has not been investigated in sufficient detail. However, our understanding of the
79	mechanism controlling the influence of metal ions on the adsorption of antibiotics is still limited. At present,
80	the main metal ions involved in these studies are $K^+$ , $Na^+$ , $Ca^{2+}$ , $Mg^{2+}$ , $Cu^{2+}$ , $Ni^{2+}$ , and $Fe^{3+}$ , whereas only few
81	investigations have focused on toxic heavy metal ions such as $Cr^{6+}$ and $Cd^{2+}[\underline{30}]$ . The microscopic
82	characterization of the interaction between metal ions and antibiotics and of the mechanism by which metal
83	ion complexation affects antibiotic adsorption is still insufficient. Activated carbon has advantages such as
84	stable chemical properties, strong adsorption capacity, low cost, and wide availability. Therefore, the study
85	of the interfacial adsorption behavior of multiple pollutants on activated carbon will support the design of
86	cost-effective adsorbents[31, 32]. For this purpose, it is necessary to explore the co-adsorption and
87	interaction mechanism of antibiotics and heavy metals on the surface of activated carbon.

88 The aim of this study is to investigate the adsorption of antibiotics (sulfamethazine, SMT) and heavy

89	metals (cadmium) in single and binary contaminated solutions, and created an ideal water model containing
90	two major contaminants: sulfamethazine and heavy metal cadmium ions. The influence of other ions in the
91	natural environment was ignored temporarily. To more clearly observe the influence of cadmium ion on the
92	adsorption capacity of SMT and the influence of complexation on the adsorption, and to observe the changes
93	on the surface and inside of the adsorbent after adsorption in a short time, a relatively large concentration
94	range of SMT and Cd <sup>2+</sup> was adopted in this study. First, we studied the adsorption behaviors of
95	sulfamethazine and cadmium ions on activated carbon in single and binary systems, based on the analysis of
96	adsorption kinetics and isotherms. Then, X-ray photoelectron spectroscopy (XPS), Raman, nuclear magnetic
97	resonance, and Fourier transform infrared (FTIR) spectroscopy techniques were used to characterize
98	adsorption changes in the binary system and the correlation between the complexation and the adsorption
99	amount. The analysis of the characterization and adsorption mechanism results allowed elucidating the
100	influence of complexation on the adsorption process, providing a comprehensive description of the
101	adsorption and interaction mechanism in the binary system.
102	
103	2. Materials and methods
104	
105	2.1 Materials
106	
107	SMT antibiotic, cadmium chloride, and activated carbon were purchased from Sigma (St. Louis,
108	Missouri, USA), Tianjin Kemeo Chemical Reagent Co., Ltd., and Taishan Chemical Plant Co., Ltd.,
109	respectively. All reagents used in this study were of analytical grade and used without further purification.

110 Deionized water was used in the experiments.

## 112 2.2 Single system adsorption experiments

114	After determining the appropriate adsorption equilibrium time and amount of activated carbon, we
115	studied the effects of these parameters on the adsorption. In the experiment, 20 mg activated carbon was
116	used in a 150 mL test solution with a constant initial SMT concentration (25 mg $\cdot$ L <sup>-1</sup> ) and sufficient contact
117	time (24 h) at 303 K. A conical flask (250 mL, glass) was shaken with a water bath thermostatic oscillator at
118	200 rpm. Samples were collected at different time intervals, and an UV-Vis spectrophotometer was used to
119	scan the whole UV region and determine the adsorption equilibrium time of SMT. The dosage of activated
120	carbon was set to 5, 10, 20, 30, and 40 mg in a 150 mL test solution with constant initial antibiotic
121	concentration (25 mg $\cdot$ L <sup>-1</sup> ) and adsorption equilibrium time (12 h), in order to determine the optimal dosage
122	of adsorbent. In the experiment, 20 mg activated carbon was used in a 150 mL test solution with a constant
123	initial $Cd^{2+}$ concentration (25 mg·L <sup>-1</sup> ) and sufficient contact time (24 h) at 303 K. A conical flask (250 mL,
124	glass) was shaken with a water bath thermostatic oscillator at 200 rpm. Samples were collected at different
125	time intervals, and inductively coupled plasma-atomic emission spectrometry(ICP-AES) was used to
126	determine the adsorption equilibrium time of $Cd^{2+}$ . We investigated the adsorption behavior of SMT and
127	Cd <sup>2+</sup> at different temperatures and carried out adsorption isotherm measurements. The temperature was set to
128	303, 313, and 323 K, and the water bath was shaken at 200 rpm under the above optimal conditions. We
129	determined the correlation between the equilibrium concentration and the adsorption capacity of SMT and
130	Cd <sup>2+</sup> at different temperatures.



134	To explore the influence of cadmium on the adsorption of SMT, different Cd <sup>2+</sup> concentrations (0, 25,
135	35, 45, 55, 65, 75, 100, 150, 350, 500, and 650 mg·L <sup>-1</sup> ) were added to a 50 mg·L <sup>-1</sup> SMT solution; then, 20
136	mg activated carbon was added and the water bath was shaken at a constant temperature (303K). To further
137	explore the adsorption behavior of SMT and cadmium ions in a binary system, we selected a concentration
138	ratio of 1:1 between antibiotic and cadmium ions. The adsorption isotherm experiments were carried out at
139	three different temperatures (303, 313, 323K).
140	
141	2.4 Characterization and analysis of AC-Cd <sup>2+</sup> -SMT ternary complex
142	
143	FTIR spectra were obtained on a vertex 70 spectrometer (Thermo Fisher, USA) to analyze the changes

144of surface functional groups before and after adsorption of activated carbon. The functional groups and 145 binding energy of elements at the surface of AC were analyzed by X-ray photoelectron spectroscopy (XPS, 146 Thermo Fisher ESCALAB 250Xi, United States), which was carried out on a Kratos Axis Ultra DLD 147 spectrometer using monochromated Al Ka X-rays at a power of 150 W. All XPS test samples were 148 freeze-dried in advance. Raman spectra were obtained by Renishaw (Hoffman Estates) equipped with 149 argon-ion laser to analyze the change of graphitization degree of activated carbon before and after the 150 adsorption. Nuclear magnetic resonance (NMR) spectroscopy (Bruker Avance 400) was used to determine 151the chemical shifts of surface elements of SMT before and after adding Cd<sup>2+</sup>.

152

153 2.5 Determination of sulfamethazine and cadmium ions

155	The concentration of sulfamethazine was determined by a UV-Vis spectrophotometer; the absorbance
156	was measured using deionized water as blank control, at a SMT maximum absorption wavelength of 261 nm.
157	The concentration of cadmium ions was determined by inductively coupled plasma-atomic emission
158	spectrometry (ICP-AES).
159	
160	2.6 Data analysis
161	
162	The adsorption capacity of sulfamethazine and cadmium ions $[q_e (mg \cdot g^{-1})]$ was calculated by equation
163	(1) [ <u>33</u> ]:
164	
165	$q_e = (C_0 - C_e) \cdot V/M \tag{1}$
166	
167	where $C_0$ and $C_e$ (mg·L <sup>-1</sup> ) are the initial and equilibrium concentrations of SMT or Cd <sup>2+</sup> before and after
168	adsorption, respectively, while $V(mL)$ and $M(mg)$ are the added volume of SMT or cadmium ion solutions
169	and the mass of activated carbon, respectively.
170	The linearized Langmuir model (Eq. (2)) and Freundlich model (Eq. (3)) were performed for the
171	adsorption isotherms of SMT and $Cd^{2+}$ to evaluate the distribution of SMT and $Cd^{2+}$ in the solid phase and
172	liquid phase after achieving adsorption equilibrium[ <u>34</u> ]:
173	
174	$C_{e'}q_{e} = C_{e'}q_{max} + 1/(K_L \hat{A} \cdot q_{max}) $ <sup>(2)</sup>
175	
176	$\ln q_e = \ln K_{\rm F} + 1/n \cdot \ln C_e \tag{3}$

178	where $q_{max}$ (mg·g <sup>-1</sup> ) is the maximum adsorption concentration of SMT and Cd <sup>2+</sup> per unit mass of AC.
179	$K_L(L \cdot mg^{-1})$ and $K_F(L \cdot mg^{-1})$ are respectively the adsorption constant of Langmuir and Freundlich models.
180	$1/n$ are the adsorption intensity constant of Freundlich. $C_0$ (mg·L <sup>-1</sup> ) is the initial concentration of SMT, and
181	the complexation ratio of SMT to $Cd^{2+}$ is 1:1[35]. The relationship between the concentration of SMT and its
182	adsorption capacity is known; the concentration of the complex can be calculated based on the concentration
183	of SMT and the complexation ratio $[35]$ , and the correlation between the complex concentration and the
184	SMT adsorption capacity can thus be determined [ $\underline{36}$ , $\underline{37}$ ].
185	
186	3. Results and discussion
187	
188	3.1 Single adsorption of SMT and Cd( II) on activated carbon
189	
190	As shown in Fig. 1a, the adsorption equilibrium time of SMT on activated carbon was approximately
191	12 h. The adsorption of SMT on AC showed no significant differences at pH 3–7. At pH 9, the effect of SMT
192	adsorption on AC was weaker than that observed under acidic and neutral conditions. As a typical
193	amphoteric compound, SMT presents different proton states (SMT <sup>+</sup> , SMT <sup>-</sup> , and SMT) at different pH
194	values[38]. When the initial pH value of the solution was 3–7, the adsorption of SMT by AC was significant.
195	This is because, at pH 3–5, SMT mainly exists as a protonated neutral molecule. At pH 5, the removal rate of
196	SMT reached 93.9%, indicating a high neutral adsorption capacity. After that, with increasing pH, the SMT

197 anion becomes the main species in the solution, the electrostatic repulsion between SMT and AC increases,

9

198 so that the adsorption capacity of SMT also decreases [39].

199	The determination of the adsorption equilibrium time of cadmium ions on activated carbon is shown in
200	Fig. 1c. The Cd <sup>2+</sup> adsorption equilibrium was reached at approximately 2 h. The results of this study are
201	generally consistent with previous reports (Figs. 1a and 1c)[18, 19, 38]. Meanwhile, this study focuses on
202	the effect of cadmium ions on the adsorption capacity of SMT, to accurately approach the typical pH value
203	of an actual water body containing SMT contaminant(pH=7), the single adsorption experiment of cadmium
204	ion and the subsequent experiments of this study were carried out under the condition of $pH = 7[40, 41]$ .
205	The effect of the AC dosage on the adsorption removal of SMT was further studied (Fig. 1b). With the
206	optimum AC dosage, the adsorption of SMT is expected to reach the maximum. The effect of the AC dosage
207	on the SMT adsorption was investigated by adding different amounts of AC to the solution. The results show
208	that the removal rate of SMT increased from 46.2% to 99.1% as the AC dosage increased from 33.33 to
209	266.67 mg·L <sup>-1</sup> , due to the increased number of adsorption sites on the adsorbent surface. When he amount of
210	AC was further increased, the removal rate of SMT remained almost unchanged, due to the decrease in the
211	adsorption capacity per unit mass of adsorbent. At higher adsorbent concentrations, the effective surface area
212	decreases, and the aggregation or overlap between adsorption sites leads to a decrease in the available
213	adsorbent surface area and an increase in diffusion path length. Some of the examined adsorbent systems fail
214	to reach adsorption saturation, which is consistent with the results of previous studies[26]. Considering
215	adsorption effects, adsorption capacity, and economic factors, the optimal adsorbent dose was estimated to
216	be 133.33 mg· $L^{-1}$ .





Fig. 2. Effect of cadmium ion concentration on adsorption of SMT.

232

233 Figs. 3a and 3b show the adsorption isotherms of SMT in the single and binary systems, respectively. The Freundlich model was more suitable for SMT adsorption (R<sup>2</sup>=0.959/0.982/0.954 for SMT with Cd<sup>2+</sup>, 234and 0.61/0.145/0.485 without Cd<sup>2+</sup>) than the Langmuir model (R<sup>2</sup>=0.942/0.94/0.949 for SMT with Cd<sup>2+</sup>, and 235 236 0.932/0.896/0.903 without Cd<sup>2+</sup>), which can be described as heterogeneous multilayer adsorption (Table 1). Compared with the system without Cd<sup>2+</sup>, the presence of Cd<sup>2+</sup> increased the adsorption capacity of SMT on 237 238 activated carbon. In particular, the addition of Cd<sup>2+</sup> significantly promoted the adsorption of SMT on 239 activated carbon, which is consistent with the results of Fig. 2a. Relevant studies have shown that organic 240 ligands bound with heavy metals can interact with functional groups on the surface of activated carbon to 241 form stable complexes [43]. Higher numbers of electron-rich groups such as N and O in antibiotics lead to a 242 stronger complexation ability with metal ions. Therefore, it can be further speculated that the organic ligands 243 bound to cadmium ions may undergo complexation reactions with the functional groups on the surface of 244 activated carbon, even though the numbers and types of different functional groups in sulfonamides are 245 limited, and the N-containing functional groups are mainly involved in the coordination [44]. The study has 246 shown that bridging by metal centers is one of the most important mechanisms for the adsorption of

antibiotics on adsorbents [26]; this may explain how  $Cd^{2+}$  can promote the adsorption of SMT on activated

248 carbon, which will be further confirmed by the experiments described in the following.

Models	Parameters		SMT		SMT(complex)		
		303K	313K	323K	303K	313K	323K
Langmuir	$q_{max}(mg \cdot g^{-1})$	216.3	215.4	201.9	266.304	257.462	253.772
	$K_L(L \cdot mg^{-1})$	3.191	9.062	2.383	1.131	1.479	1.375
	R <sup>2</sup>	0.61	0.145	0.485	0.922	0.92	0.919
Freundlich	$K_F(L \cdot mg^{-1})$	8.329	9.069	9.235	8.732	7.219	6.251
	n	0.665	0.716	0.793	0.699	0.809	0.803
	R <sup>2</sup>	0.979	0.929	0.919	0.959	0.982	0.954

Table 1 Calculated Langmuir and Freundlich parameters of SMT adsorption isotherms

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Figs. 4a and 4b show the adsorption isotherms of  $Cd^{2+}$  in the single and binary system, respectively. The adsorption amount of  $Cd^{2+}$  decreased after SMT was added to the system. This can be explained by assuming that the adsorption of  $Cd^{2+}$  was inhibited by the complexation with SMT, which thus reduced the

257	adsorbed Cd <sup>2+</sup> amount. The addition of cadmium ions initially promoted the adsorption of SMT; however,
258	when the Cd <sup>2+</sup> concentration was further increased, no further increase in SMT adsorption was observed.
259	This suggests a monolayer adsorption behavior of cadmium ions on activated carbon, which cannot further
260	promote the adsorption of SMT at higher Cd <sup>2+</sup> concentrations[25]. The Langmuir model was more suitable
261	for $Cd^{2+}$ adsorption (R <sup>2</sup> =0.959/0.999/0.966 for $Cd^{2+}$ with SMT, and 0.985/0.989/0.991 without SMT) than
262	the Freundlich model ( $R^2$ =0.932/0.926/0.903 for $Cd^{2+}$ with SMT, and 0.932/0.896/0.903 without
263	SMT)(Table 2). When the atomic sites on the surface of activated carbon are unsaturated, $Cd^{2+}$ will be
264	adsorbed on the surface. After the adsorption of one layer of $Cd^{2+}$ ions, the original unsaturated sites become
265	saturated, and no further adsorption on the activated carbon is possible. Due to the strong interaction
266	between the functional groups on the surface of activated carbon and $Cd^{2+}$ , the adsorption of the latter tends
267	to be uniform, resulting in a single-layer covering. This is consistent with the Langmuir isotherm model of
268	monolayer adsorption [ $45$ ].

 Table 2 Calculated Langmuir and Freundlich parameters of Cd<sup>2+</sup> adsorption isotherms

Models	Parameters	$\mathrm{Cd}^{2+}$			Cd <sup>2+</sup> (complex)		
		303K	313K	323K	303K	313K	323K
Langmuir	$q_{max}(mg \cdot g^{-1})$	59.6	88.55	81.2	32.744	22.036	36.455
	$K_L(L \cdot mg^{-1})$	0.216	0.318	0.497	0.315	0.357	0.418
	R <sup>2</sup>	0.985	0.989	0.991	0.959	0.999	0.966
Freundlich	$K_F(L \cdot mg^{-1})$	2.528	2.324	2.084	2.098	2.097	2.098
	n	0.464	0.421	0.452	0.451	0.453	0.469
	R <sup>2</sup>	0.932	0.896	0.903	0.932	0.926	0.903



Fig. 4. Adsorption isotherms of Cd( II) in single (a) and binary (b) systems, along with Langmuir model fits.

272

275	3.3 Effect of	complexation	on co-adsorpt	tior

276

#### 277 3.3.1 FTIR analysis of adsorption mechanism

278 FTIR spectroscopy was used to determine changes in the surface functional groups before and after adsorption. And the FTIR spectra of Cd<sup>2+</sup>, SMT and SMT+Cd<sup>2+</sup> adsorbed on activated carbon were 279 280 compared (Fig. 5). In the a-d spectra(Fig.5), the peak at 3445 cm<sup>-1</sup> is the characteristic peak of -OH (from 281 phenol or alcohol) and the tensile vibration of water adsorbed on AC [46, 47]. The peak at 1412 cm<sup>-1</sup> is the 282 stretching vibration band of C-O-C, C=C, or C-H on the surface of activated carbon [47, 48], the 283 characteristic peak at 1613 cm<sup>-1</sup> may be attributed to the C=O tensile vibration on the AC surface [46, 47]. 284 The peak at 1638 cm<sup>-1</sup> indicated that the band has the characteristic of aromatic ring stretching mode. After 285 SMT was adsorbed on AC (c, d spectrum, Fig.5), there are one or more aromatic rings in the AC structure, 286 corresponding to the pyrimidine ring structure and aromatic ring in SMT [46]. And there is an obvious 287 characteristic peak at 3234 cm<sup>-1</sup>, which may correspond to the stretching vibration of -OH [48]. In the b, d 288 spectra (Fig. 5), the peak at about  $1105 \text{ cm}^{-1}$  was significantly enhanced, which is a strong characteristic 289 peak for the adsorption of heavy metal Cd<sup>2+</sup> [49]. Under neutral conditions, SMT mainly exists in the form of SMT<sup>0</sup> and SMT<sup>-</sup> [50]. When Cd<sup>2+</sup> was added, the H part on the Sulfonamide group is ionized to form a 290 negatively charged SMT, which can be complexed with Cd<sup>2+</sup> by replacing H<sup>+</sup> [51, 52]. Therefore, in the 291 292 spectrum d (Fig. 5), the significant fluctuations at 3234cm<sup>-1</sup>-3445cm<sup>-1</sup> indicated that it is the vibration and fracture of -NH in SMT, which complexes with  $Cd^{2+}$  by substituting H at the N atom[53]. After  $Cd^{2+}$  was 293 adsorbed on AC, new characteristic peaks appeared at 2937cm<sup>-1</sup> and 2866cm<sup>-1</sup>, and this change was still 294observed in AC-Cd<sup>2+</sup>-SMT samples, indicating the formation of AC-Cd<sup>2+</sup>-SMT ternary complex [49]. At the 295same time, the outermost shell of the Cd<sup>2+</sup> nucleus had an empty orbital that can accommodate lone pair 296 297 electrons, while oxygen, sulfur, nitrogen, and other atoms are typical lone pair electron donors [54]. It can be 298 speculated that the N atoms in the pyrimidine ring participate in the complexation process. The analysis of 299 the structure of the SMT molecule suggested that multiple interactions can be involved in the complexation







Fig. 5. FTIR spectra of (a) AC before adsorption, (b) Cd( II)-adsorbed AC, (c) SMT-adsorbed AC, and (d)

#### SMT/Cd( II)-adsorbed AC.

304

### 305 3.3.2 XPS analysis of adsorption mechanism

306 **Table 3** 

	3(	07	Elemental com	position of AC.	SMT-adsorbed AC	, Cd( 🛛	)-adsorbed AC	, and SMT/Cd(	Π	)-adsorbed AC
--	----	----	---------------	-----------------	-----------------	---------	---------------	---------------	---	---------------

Name	Elemental analysis (atom based) (%)					
	С	0	N	S	Cd	
AC	91.89	7.41	0.7	a	a	
AC-SMT	85.89	8.79	4.29	1.03	a	
AC-Cd(II)	92.09	6.93	0.85	a	0.13	
AC-Cd(I)-SMT	84.38	7.7	5.81	1.97	0.15	

308 <sup>a</sup> not detected.

309

310 As shown in Fig. 6a, the XPS profile of the single AC sample shows typical C1s and O1s peaks at 311 284.8 and 532.6 eV. After adsorption of Cd(II), a Cd3d peak at 416.54 eV appears in the XPS profile, and 312 Table 1 shows a percentage of Cd(II) compared with the AC sample, indicating that Cd metal ions were adsorbed on the adsorbent surface. The adsorption of Cd<sup>2+</sup> mainly relied on the electrostatic attraction 313 between AC surface and Cd<sup>2+</sup> due to deprotonation[33], which proves that there was some kind of binding 314 315 interaction between them. SMT co-adsorption led to the simultaneous appearance of N1s and S2p peaks, as 316 shown in Fig. 6a. Compared with the AC sample, the N content in the AC-SMT system was significantly higher, confirming that SMT was adsorbed on the surface. The N content further increased in the ternary 317 system, which indicates that the presence of Cd<sup>2+</sup> promotes the adsorption of SMT. Cadmium ions are first 318

adsorbed by cation- $\pi$  interactions and then diffuse to other adsorption sites. Although the cation- $\pi$  interaction does not promote the adsorption of SMT, cadmium species adsorbed at other sites may form SMT-Cd<sup>2+</sup>-AC complexes with negatively charged SMT, and Cd<sup>2+</sup> ions at a certain concentration can enhance the adsorption of SMT[55].

- The N1s peak decomposes into two related peaks: N-C=N(399.3eV) and -NH(400.6eV)(Figs.5b and Sc) [56]. According to the peak area calculation of Fig.5b and Fig.5c, it can be concluded that the -NH part of the system is reduced (the peak area is reduced from 1307.15 to 1198.3) with the addition of  $Cd^{2+}$ . Moreover, the binding energy of -NH shifted from 400.6eV to 400.71eV, while that of N-C=N shifted from 399.3eV to 399.24eV. It is revealed that -NH in SMT is the main functional group involved in complexation,
- 328 and N on the pyrimidine ring may also participate in complexation [ $\underline{49}$ ].

329 As shown in Fig. 6d, the binding energies of Cd(II) adsorbed in the binary system were shifted to 330 lower values, showing that the changes in chemical bonding after adsorption on AC in the binary system 331 resulted in a red shift of the XPS signals relative to those of the single heavy metal system. This means that 332 the metal ions are in their reduced state in the presence of SMT[33]; the electrons involved in the reduction 333 process are generated from the breaking of the N-H bond of SMT, which indicates that the metal cations 334 interact with the N atoms (acting as electron donors) to form a complex after the N-H bond cleavage (Figs. 335 5b and 5c). This is consistent with the previous FTIR spectroscopy results. The atomic percentages obtained 336 from the peak areas show that the metal ions enhanced the adsorption of SMT (from 4.29% to 5.81%; Table 3), which is consistent with the adsorption isotherm experiments obtained for the SMT- $Cd^{2+}$  system (Fig.3b). 337 Therefore, at a certain concentration of Cd<sup>2+</sup>, the AC-Cd<sup>2+</sup>-SMT ternary complex is formed through metal 338 339 cation bridging. The cadmium ion acts as a bridge, indirectly connecting SMT with the adsorbent [57]. In the 340 absence of cadmium ions, the surface functional groups of SMT molecules and adsorbents are negatively

341 charged. The corresponding electrostatic repulsion impairs the adsorption performance of activated carbon.
342 The presence of cadmium ions effectively reduces the electrostatic repulsion between SMT and activated
343 carbon. The small hydration radius of cadmium ions results in a strong ability to form coordination
344 complexes with SMT under neutral conditions. Hence, the bridging effect of Cd cations is relatively strong,
345 which provides more adsorption sites for SMT in water; this can promote the adsorption of SMT, thus
346 improving the efficiency of its removal process[58].



349 Fig. 6. (a) Full-scan XPS profiles of AC before adsorption (1), SMT-adsorbed AC (2), Cd( II)-adsorbed AC (3), and



351 SMT/Cd(II)-adsorbed AC; (d) Cd3d binding energy change between single and binary systems.

352

353 3.3.3 Raman and NMR analysis of adsorption mechanism

354	The Raman spectra of the four solids (Fig. 7) show two peaks. The first, near 1595 $\text{cm}^{-1}$ (G peak, sp <sup>2</sup>
355	C), is the characteristic scattering peak of graphite, whereas the second peak at 1350 cm <sup>-1</sup> (D peak, sp <sup>3</sup> C) is
356	due to lattice defects, disorder, and low-symmetry sites in the carbon structure of graphite[59]. The Raman
357	intensities are related to the structural order of the carbon sheets. The ID/IG ratio (where ID and IG are the
358	intensities of the D and G peaks, respectively) is sensitive to the graphitization degree, which is the
359	parameter used to measure the defect density of activated carbon[60]. Therefore, the graphitization degree of
360	a carbon material can be evaluated using the $R = ID/IG$ parameter. A smaller R value corresponds to a higher
361	degree of graphitization[61]. The ID and IG values are obtained by calculating the peak areas of peak D and
362	peak G, and the relative intensity ratio of ID/IG is obtained [62]. The R values of the four Raman spectra
363	were 2.06 (AC), 2.20 (AC-Cd <sup>2+</sup> ), 1.98 (AC-SMT), and 1.936 (AC-SMT/Cd <sup>2+</sup> ). The D band at 1350 cm <sup>-1</sup> is a
364	defect-induced feature, which reflects the imperfect crystal structure of carbon. Compared with AC, the
365	ID/IG value of the AC-Cd <sup>2+</sup> system increased from 2.06 to 2.2, which indicates that more structural defects
366	were formed on Cd <sup>2+</sup> -doped AC[63], resulting in a more disordered AC structure. However, the ID/IG
367	values of SMT and SMT/Cd <sup>2+</sup> decreased from 2.06 to 1.98 and 1.936, respectively, indicating a reduced
368	defect density and higher graphitization degree of carbon. This type of activated carbon substrate will
369	provide more binding sites for the adsorption process; in other words, the high degree of graphitization can
370	promote the adsorption process [ $64$ ], thus enhancing the adsorption of SMT, up to a certain extent [ $48$ ]. In
371	agreement with the above FTIR analysis, with the enhanced SMT adsorption, the formation of the $Cd^{2+}$ -SMT
372	complex on the activated carbon surface promoted the adsorption of SMT.
373	As the hydrogen atoms of amino groups on the benzene ring are highly active, they are likely to be
374	replaced by deuterium in a deuterated solution [36, 65, 66]; hence, it is difficult to observe the corresponding

peak in the NMR spectra in Fig. 8. The first peak, which is located at high fields (2–3 ppm) and exhibits a

376 large integral, corresponds to the four hydrogen atoms in the benzene ring. The second signal is a single peak 377 at 5 ppm, corresponding to the hydrogen of the -NH- group connected to the pyrimidine ring; the third peak, 378 with a chemical shift of 6-8 ppm, corresponds to three hydrogen atoms on the pyrimidine ring. The presence 379 of cadmium ions results in an obvious decrease in the intensity of the four-hydrogen peak on the benzene 380 ring, and the corresponding signal partially disappears; moreover, the signal of the hydrogen atom in the 381 -NH- group connected to the pyrimidine ring also disappears. This behavior could be attributed to the 382 breaking of the N-H bond and the complexation of Cd(I). In addition, the third peak at 6-8 ppm, 383 corresponding to the hydrogen atoms in the pyrimidine ring, almost disappears. It can be concluded that, after adding Cd<sup>2+</sup>, part of the hydrogen atoms on the pyrimidine ring will be ionized, and their corresponding 384 385 signal will thus disappear.





387 Fig. 7. Raman spectra of (a) AC before adsorption, (b) SMT-adsorbed AC, (c) Cd( II)-adsorbed AC, and (d)

#### SMT/Cd( II)-adsorbed AC.

389



401 capacity of SMT was plotted in Fig. 9, a linear regression analysis was performed, which highlights a good

402 correlation between the concentration of  $Cd^{2+}$ -SMT and the SMT adsorption amount ( $R^2 = 0.84164$ )[37].

403 These results show that the complexation of  $Cd^{2+}$  and SMT has a significant effect on the adsorption of SMT



- 419 promotes the adsorption of SMT on activated carbon, acting as a bridge (as shown by XPS) indirectly
- 420 connecting SMT with the adsorbent[58]. The bridging effect of cadmium ions improves and promotes the

- adsorption of SMT. As the adsorption of cadmium ions on activated carbon occurs in monolayer mode, when
- their concentration is increased above the monolayer (reaching the adsorption equilibrium), the Cd ions
- cannot further promote the adsorption of SMT, whose improvement is thus limited[25].



- affects the adsorption capacity of activated carbon. The adsorption by AC in alkaline conditions (pH = 9) is

weaker than that in acid conditions. The adsorption capacity of SMT decreases with increasing adsorbentdosage, while the removal rate increases.

436 In the SMT-Cd<sup>2+</sup> co-adsorption system, as the cadmium ion concentration is increased, the synergistic 437 effect of Cd<sup>2+</sup> on the transport of SMT on activated carbon promotes its adsorption. The SMT adsorption 438 data conform to the Freundlich isotherm model, indicating the multilayer heterogeneous adsorption behavior 439 of SMT on AC. On the other hand, the adsorption of cadmium on AC can be described by the Langmuir 440 isotherm model, which suggests monolayer adsorption; therefore, no further promotion of SMT adsorption 441 can be achieved when the concentration of cadmium ions is increased above the monolayer coverage. 442 The characterization analysis showed the formation of a ternary AC-Cd<sup>2+</sup>-SMT complex at a certain 443 concentration of Cd<sup>2+</sup>. Cadmium act as a bridge indirectly connecting SMT with activated carbon, providing 444 further adsorption sites for SMT molecules in water. At the same time, the presence of cadmium ions 445 effectively reduces the electrostatic repulsion between SMT and activated carbon, thus promoting the 446 adsorption of SMT. Moreover, under neutral conditions, the complexation of  $Cd^{2+}$  with SMT shows a strong correlation with the SMT adsorption amount ( $R^2 = 0.84164$ ). Overall, the present results show that the 447 448 formation of a Cd<sup>2+</sup>-SMT complex has a significant effect on the adsorption of SMT. The current study also 449 emphasizes that, for a better understanding of the ecological risks associated with a pollutant, any 450 assessment of its environmental behavior should take into account the presence of other pollutants.

451

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